

Large-Eddy simulation of a certification burner with fully coupled conjugate heat transfer

GRT ACCORT – Centrale Supélec
22/11/2018

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Collaboration: **SAFRAN Helicopter Engines**
(N. CHAUVET, S. DIDORALLY)



Motivation

❖ Context

- Manufacturers need to certify equipments in terms of fire resistance (housing, fastening engine, ...)
- Certification: the apparatus needs to be submitted [1]
 - to a kerosene / air burner
 - during a fixed time (5 to 15 minutes)
 - with a standardized flame: 1100°C ($\approx 1300\text{K}$) and 116 kW/m^2
 - This can be **VERY** expensive...



Liquid-fuel burner

❖ Purpose

- Model fire resistance tests with Large-Eddy Simulation (LES)
- Improve comprehension of phenomena involved in tests
 - Characterize inhomogeneities inside the torch (burnt gases, droplets)
- Perform many **NUMERICAL** certification tests
- Try to minimize the number of **REAL** certification tests



❖ Difficulties

- Very different time and space scales
- Multi-physics and complex geometry
- Very few studies

Large-Eddy Simulation

[1] T. Poinso, D. Veynante (2005). RT Edwards
[2] B. Abramzon, W.A. Sirignano (1989). Int J Heat Mass Transfer
[3] P. Dagaut, M. Cathonnet (2006). Progress Energy & Comb Sci
[4] L. Guedot (2014). ERCOFTAC ETMM 10

❖ Large-Eddy Simulation [1]

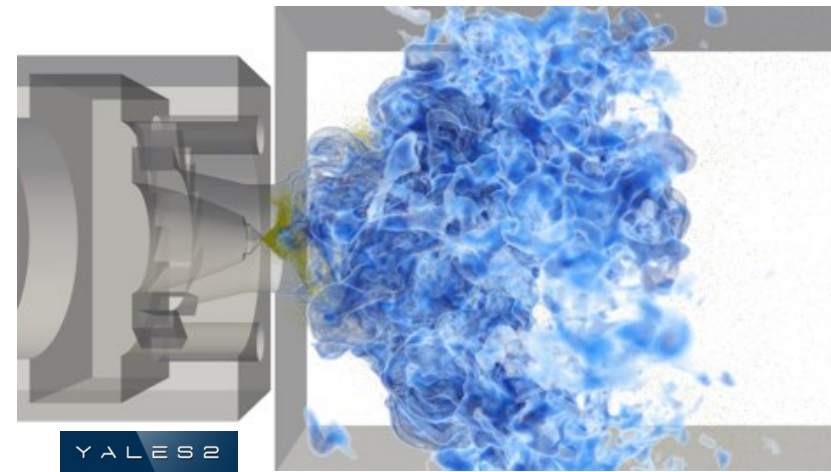
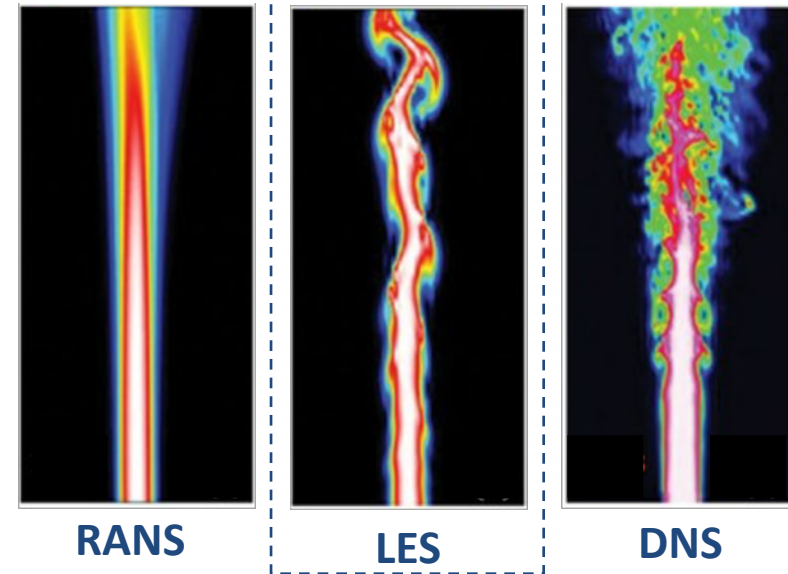
- Filter Navier-Stokes equations
- Transport of large scales
- Modelling of small scales
- Well adapted to unsteady phenomena

❖ Models for combustion in aero engines

- Two phase flow (liquid fuel) [2]
- Detailed chemistry (a lot of reactions) [3]
- Crude models for heat transfer
 - Few studies with Conjugate Heat Transfer (CHT)
 - No Radiative Heat Transfer

❖ Objectives of the present study

- Progress on HT modelling
 - Convection
 - Conduction
 - Radiation
- Validate the models
- Investigate their impact in an industrial system



MERCATO combustion chamber [4]

I. Model and coupling strategies

II. Academic validation

III. Torch flame results



Fluid solver: YALES2 [1]

- ❖ Low-Mach Number Navier-Stokes equations
- ❖ Finite Volumes on unstructured meshes
- ❖ Dedicated to DNS & LES of Multiphysics Flows
 - ❖ Turbulence
 - ❖ Combustion
 - ❖ Two-phase flows (droplets, bubbles, liquid sheets, ...)
- ❖ High-order schemes (centred 4th) → low dissipation and dispersion
- ❖ In house linear solver: Deflated PCG [2] for symmetric systems
- ❖ Designed for HPC: scale-up to 10^{10} cells and 10^5 cores
- ❖ More than 200 users across Europe, both industry and academic
- ❖ More than 80 publications related to YALES2 (Google Scholar)
- ❖ 2011 IBM Faculty award

Fluid solver: YALES2

❖ 3 main maintainers

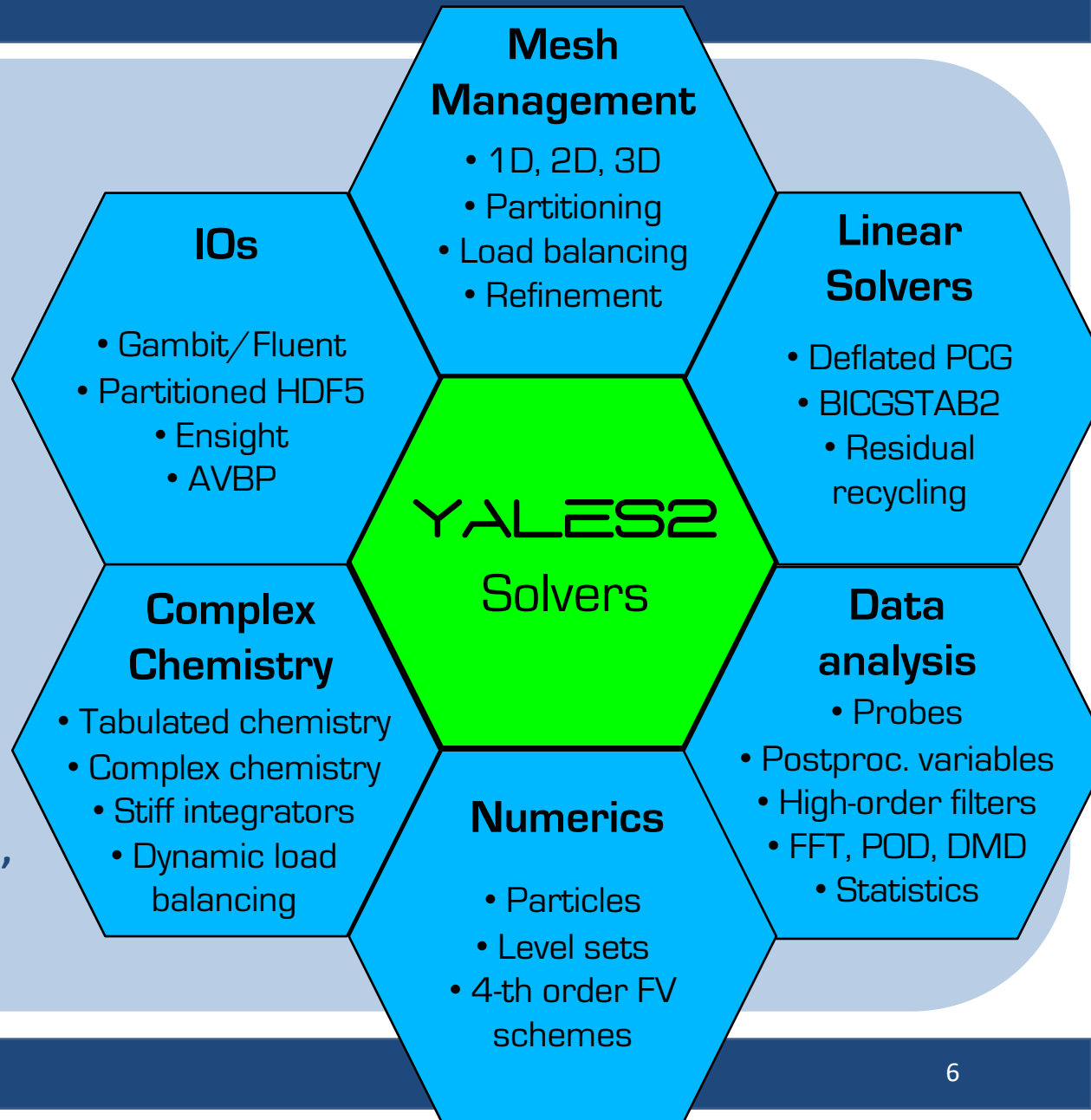
- V. Moureau
- G. Lartigue
- P. Bénard

❖ 430 000 lines of object-oriented f90

❖ Python interface

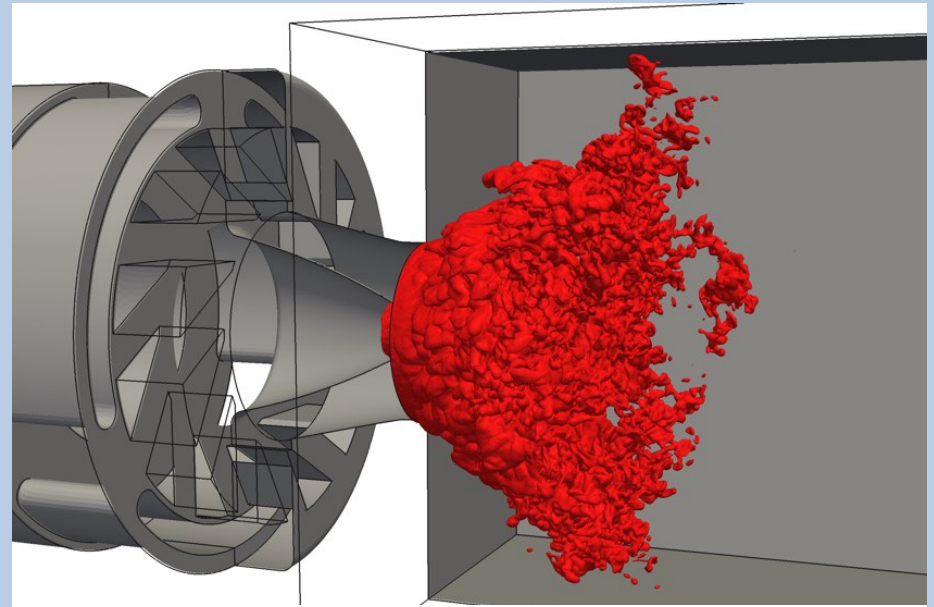
❖ Git

❖ Portable on all the major platforms + ARM, Xeon Phi, ...



❖ Solvers list

- Scalar solver (SCS)
- Level set solver (LSS)
- Lagrangian solver (LGS)
- Incompressible solver (ICS)
- Variable density solver (VDS)
- Spray solver (SPS)
- Magneto-Hydrodynamic solver (MHD)
- Heat transfer solver (HTS)
- Chemical reactor solver (CRS)
- Linear acoustics solver (ACS)
- Mesh movement solver (MMS)
- ALE solver (ALE)
- Radiative HT solver (RDS)
- Explicit compressible solver (ECS)
- Implicit compressible solver (CPS)
- Immersed boundary solver (IBS)
- Darcy solver (DCY)
- Granular flow solver (GFS)
- ...



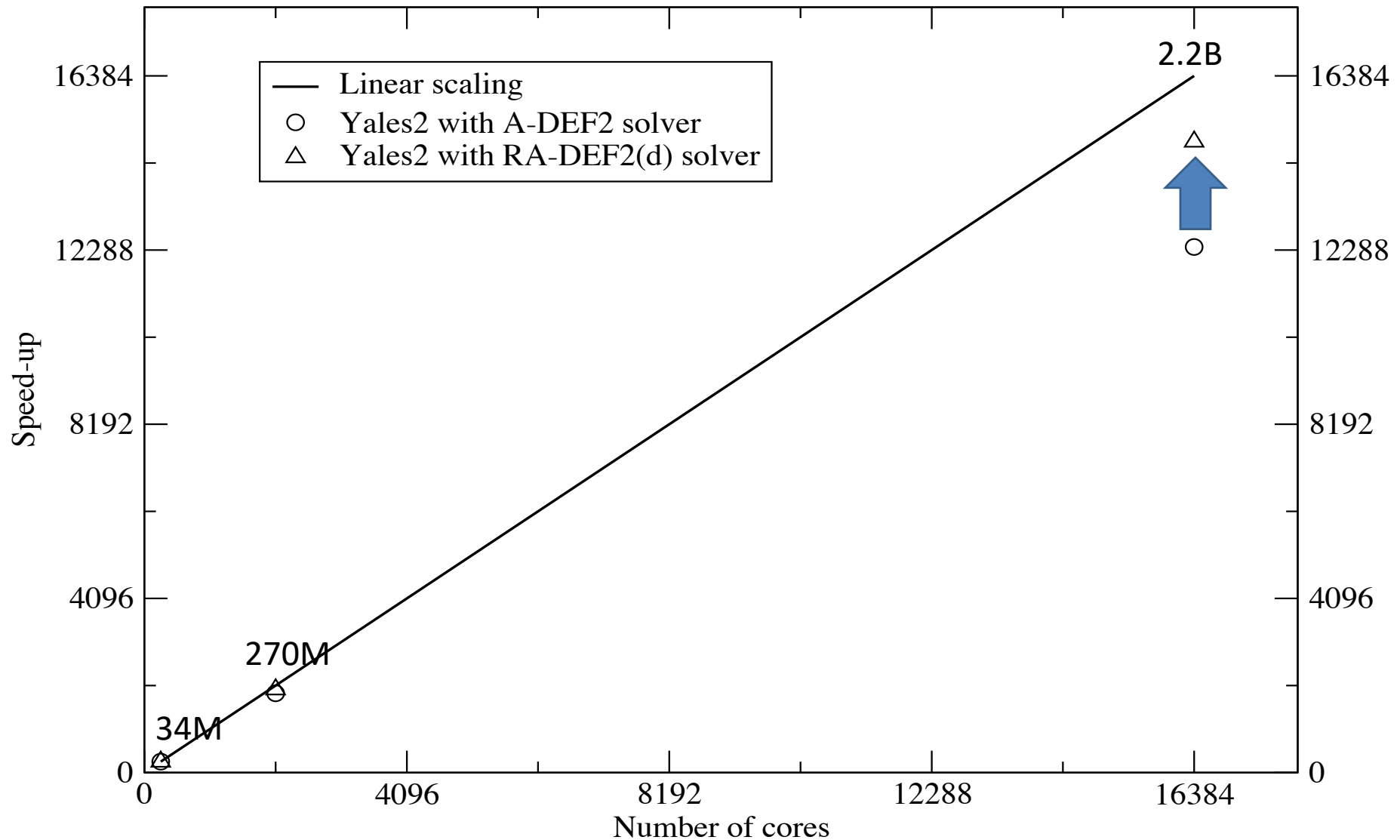
PRECCINSTA Burner
2.6 billion cells, 16384 cores of BG/P

More details:

- www.coria-cfd.fr
- www.youtube.com/user/CoriaCFD

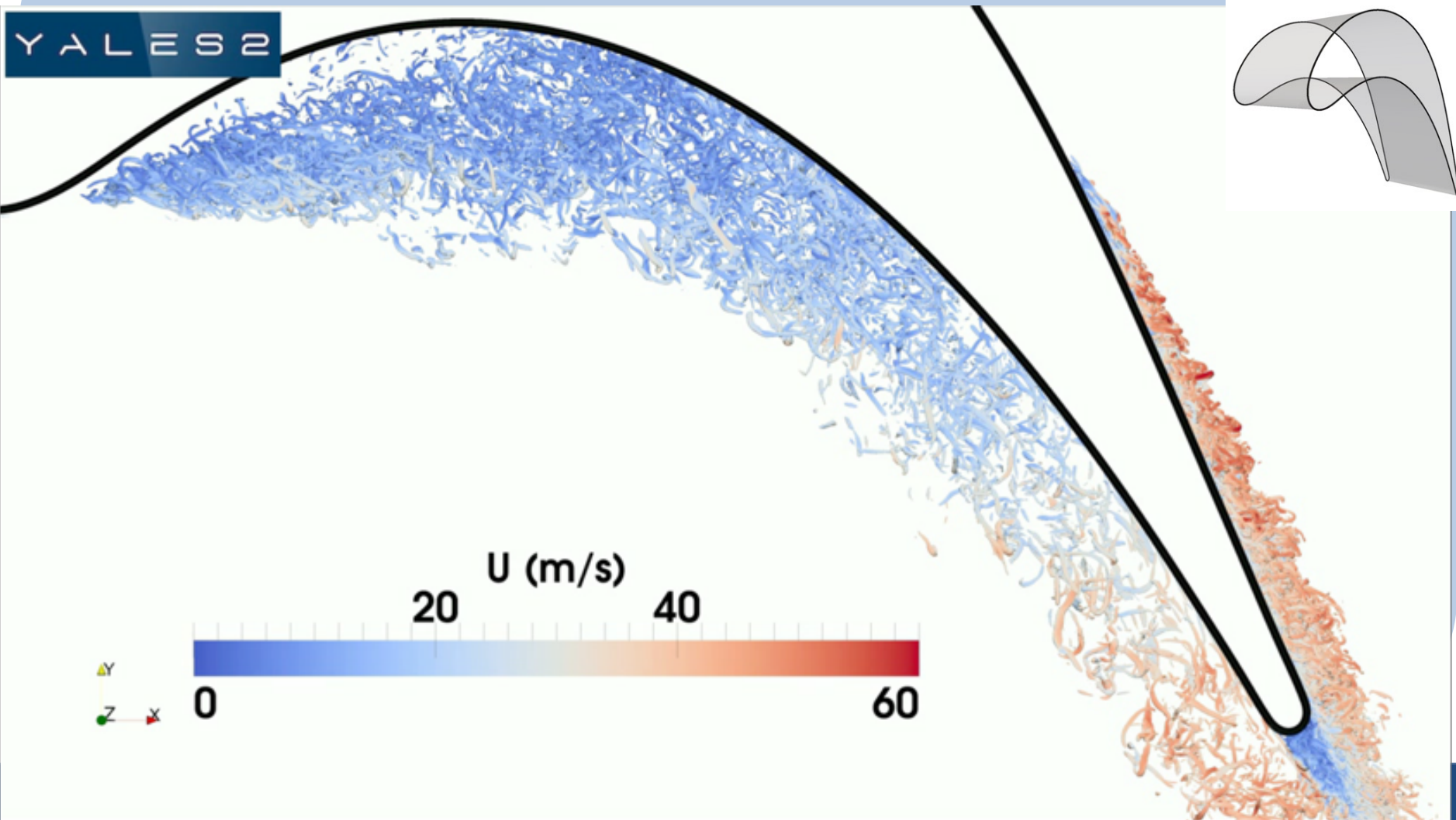
Fluid solver: YALES2

❖ Speed-up of the YALES2 incompressible solver on Curie (TGCC-CEA)



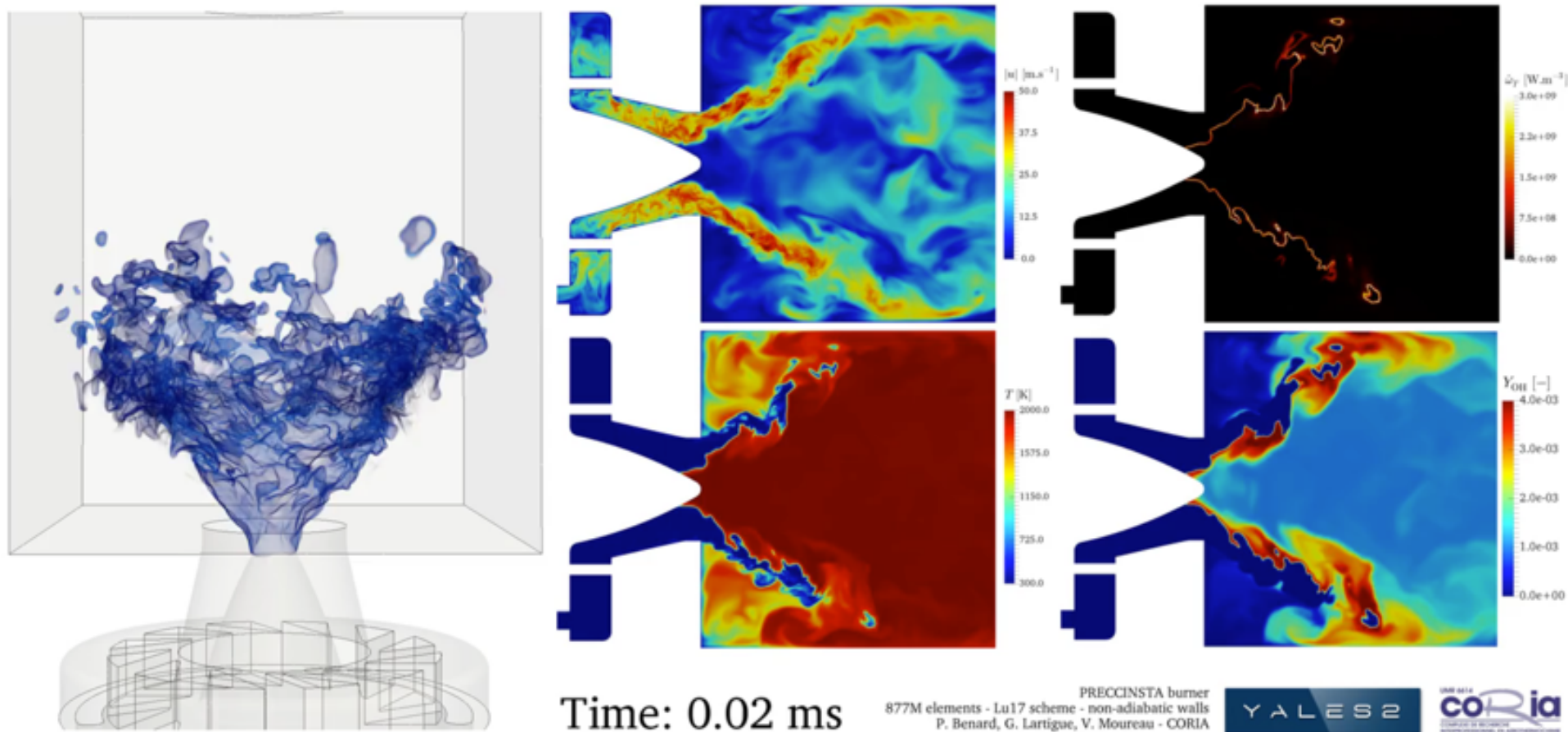
Fluid solver: YALES2

- ❖ Visualisation of the vortices cores by iso Q-criterion colored by velocity
- ❖ 2.2B cells on 16'384 cores

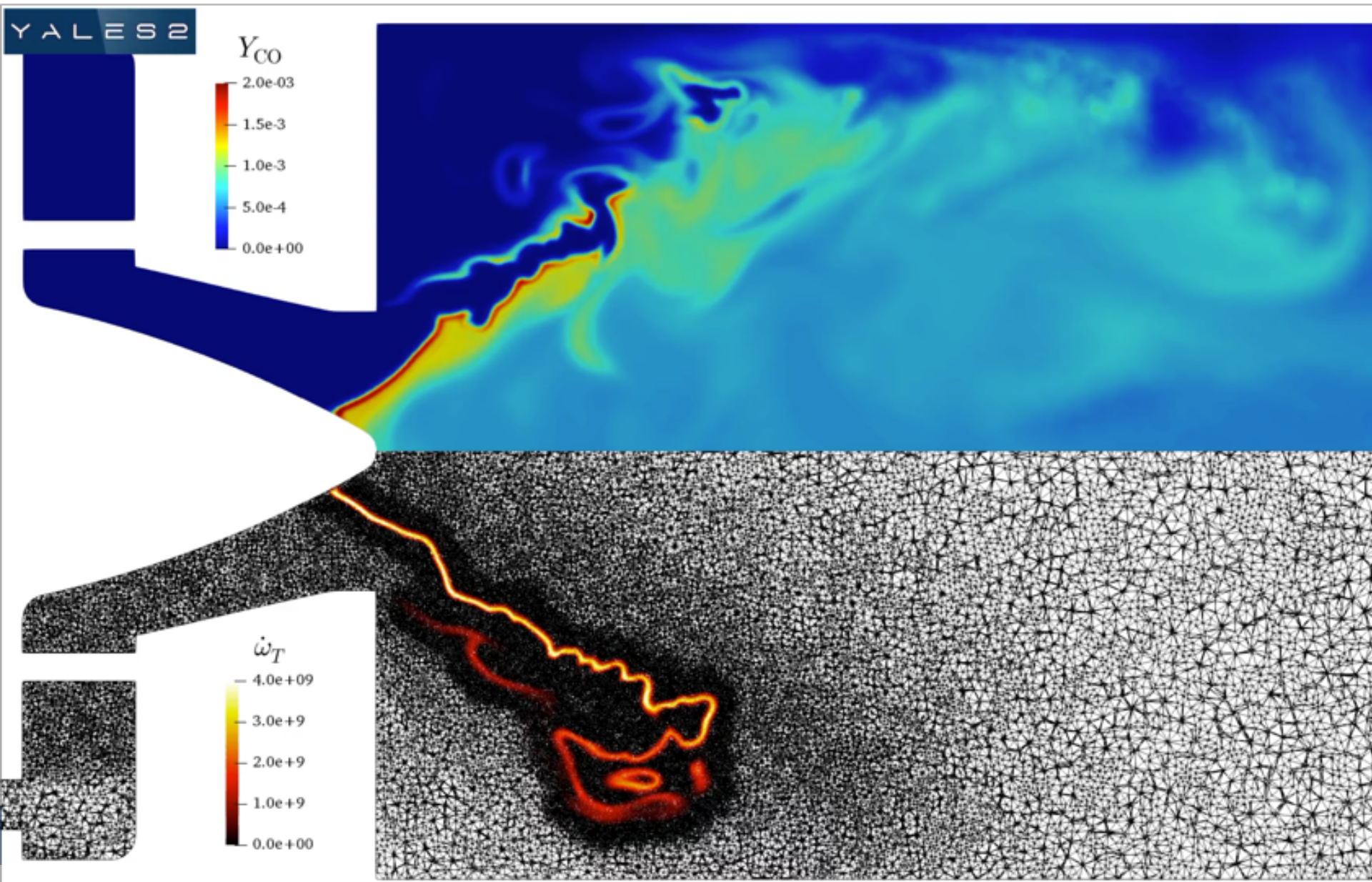


Fluid solver: YALES2

- ❖ Computation of the PRECCINSTA semi-industrial burner with YALES2
- ❖ Quasi-DNS ($\Delta x = 50\mu\text{m}$ in the flame) with complex chemistry (Lu17 scheme)
- ❖ Including Wall Heat Losses
- ❖ 877M cells / 10'000 processors

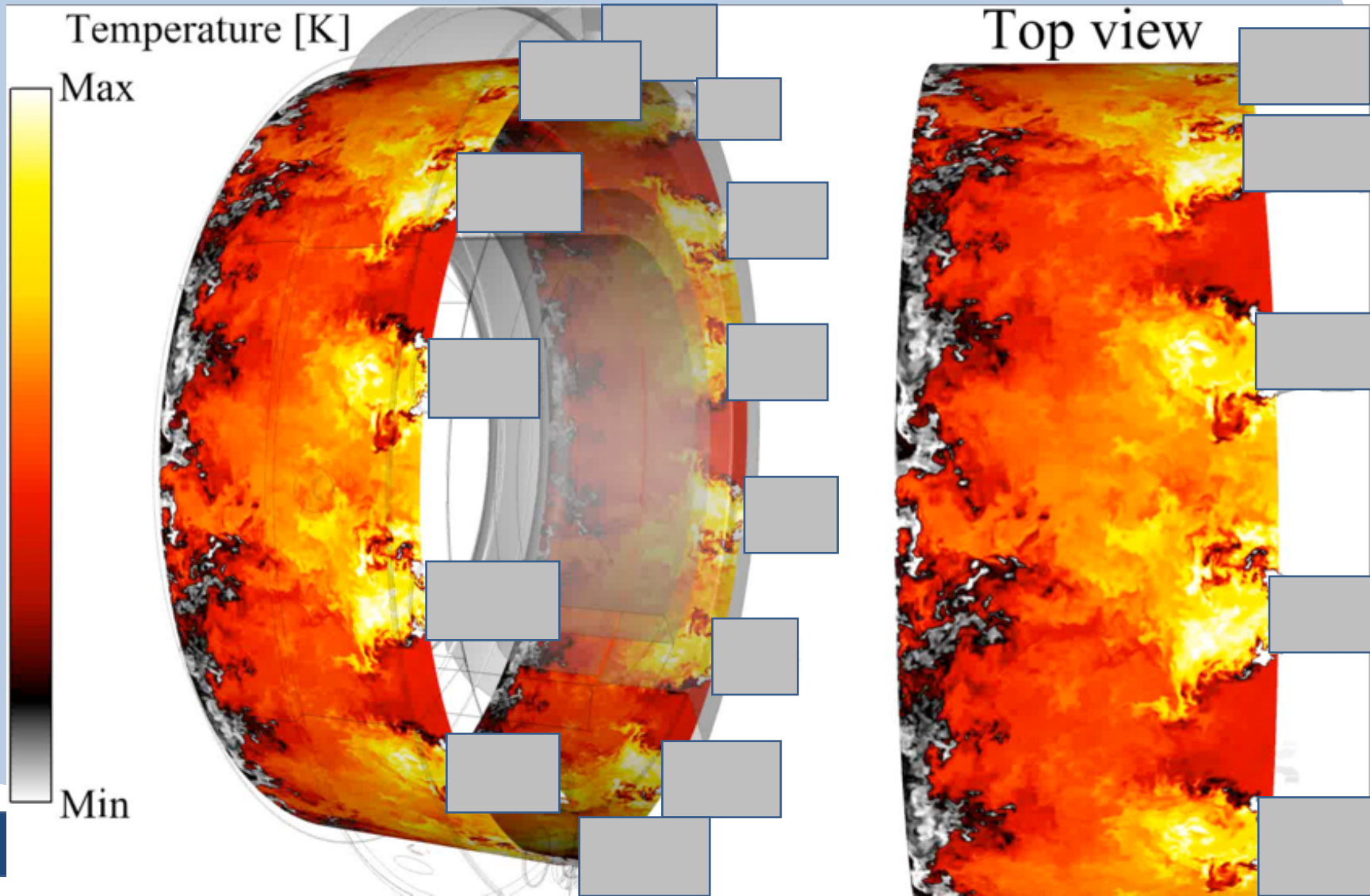


Fluid solver: YALES2



Fluid solver: YALES2

- ❖ LES of a Low-NO_x combustor (courtesy Safran HE) with 376M cells

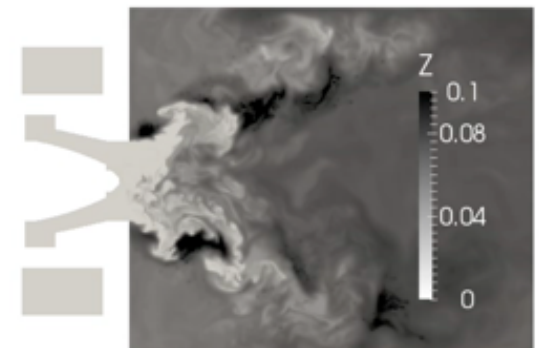
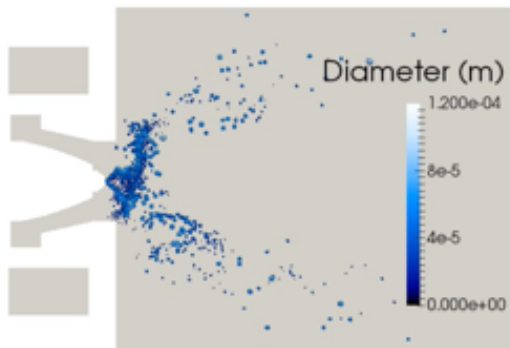
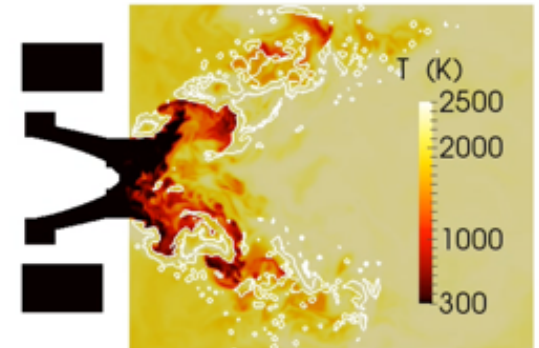
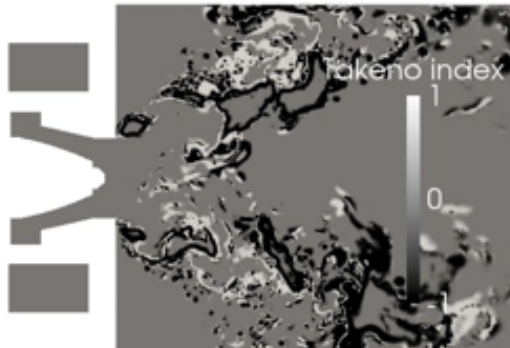
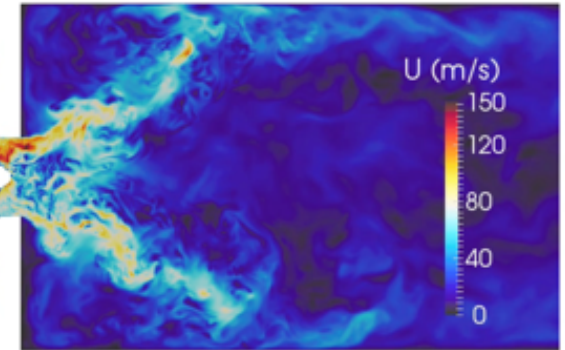
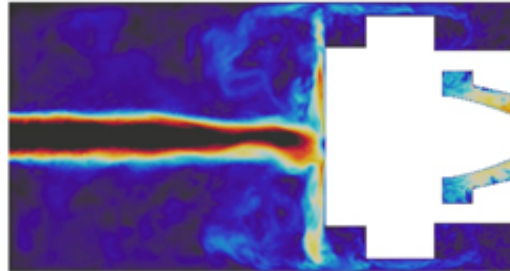
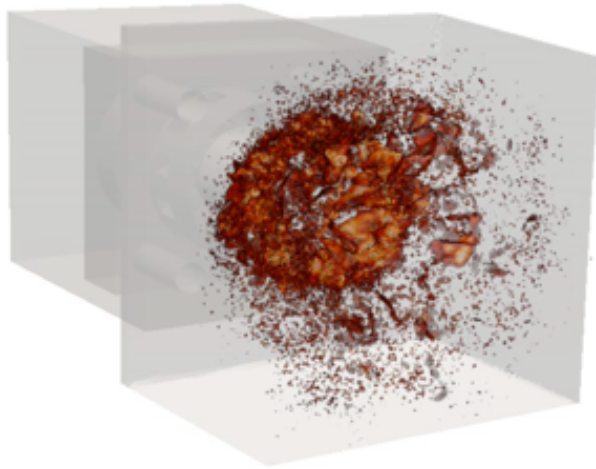


Fluid solver: YALES2

❖ LES of the atomization and combustion of a kerosene injector with 320M cells

MERCATO - 320M cells - 4096 procs OCCIGEN

Time : 0.00 ms



UMR 6614
coRia
COMPLEXE DE RECHERCHE
INTERPROFESSIONNEL EN AÉROTHÉRAUSTIQUE

YALES2



INSA

INSTITUT NATIONAL
DES SCIENCES
APPLIQUÉES
ROUEN

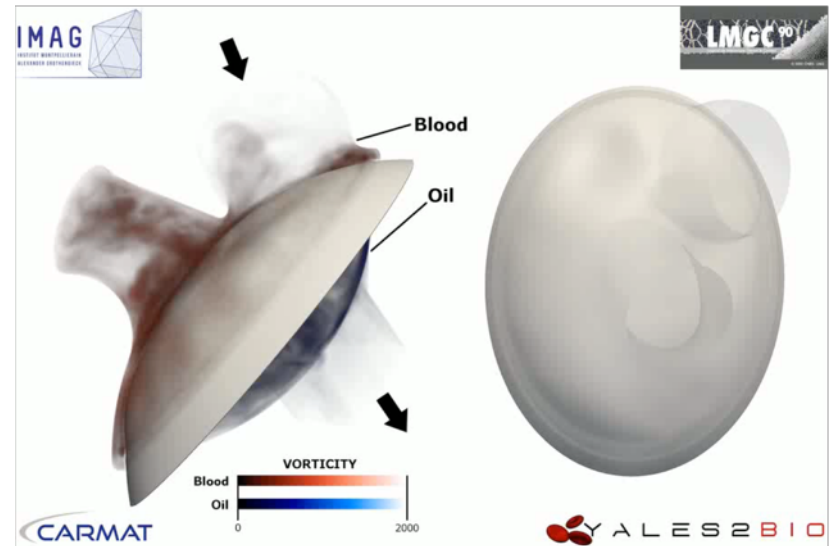
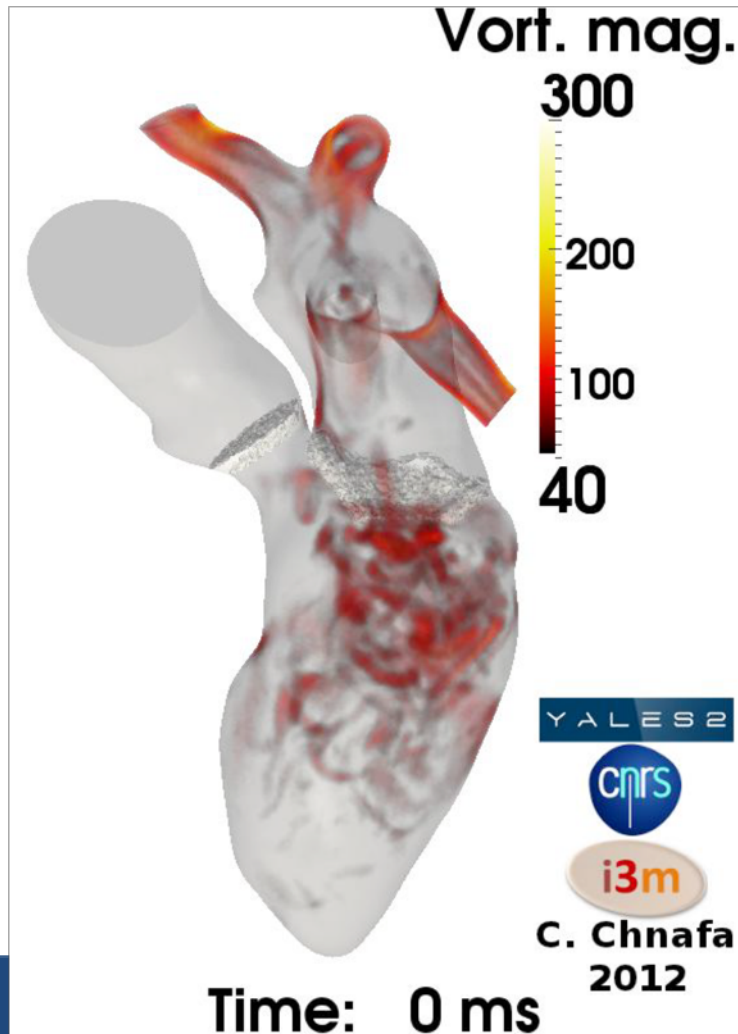


Normandie Université

Some studies with



- ❖ Project led by S. Mendez and F. Nicoud at IMAG, Montpellier



The YALES2 Team

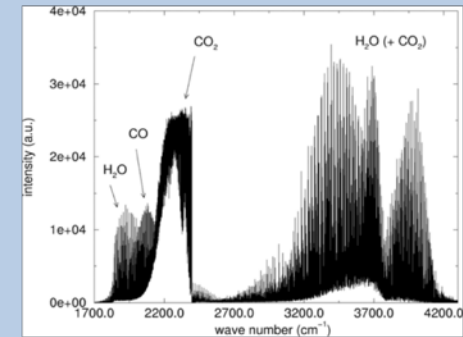


Coupling strategy: solver interactions

- [1] V. Moureau (2011). Combustion & Flame
- [2] http://www.cerfacs.fr/globc/PALM_WEB/
- [3] M.B. Giles (1997). Int. journal for num methods in fluids
- [4] F. Duchaine (2009). Int Journal of Heat & Fluid Flow
- [5] A. Felippa (2001). Comput. methods in appl mech & eng
- [6] M.F. Modest (2013). Academic Press

CHT

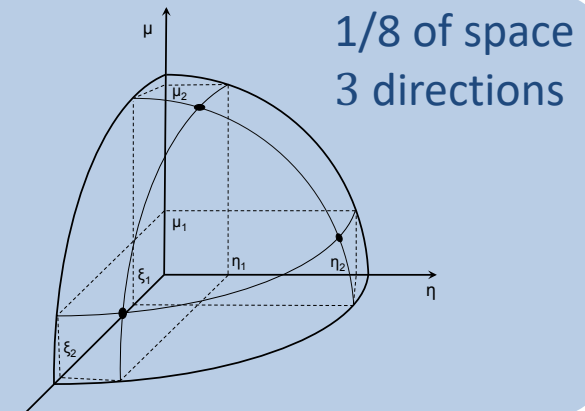
- ❖ **Fluid** and **Solid** have to **communicate**
 Solver: **YALES2** [1]
 Coupling: **OpenPALM** [2]
- ❖ **What is exchanged?** [3,4]
 - **Fluid** side: **Flux** is sent
 - **Solid** side: **T** is sent
- ❖ **How? Parallel Asynchronous Coupling Strategy** [4,5]



Emission spectrum (CH₄/air flame, 2160K)

Radiation

- ❖ **Importance of radiation in combustion**
 - High temperatures
 - Burnt gases: high absorption power
- ❖ **Solve Radiative Heat Transfer Equation** [6]
 - Spectral quadrature
 - **Angular quadrature (DOM)**
 - Spatial discretization **SAME MESH as Fluid**



1/8 of space
3 directions



Radiative solver: gas properties

- [1] Goody (1989). J. Quant. Spectro. & Radiative Transfer
- [2] Lacis & Oinas (1991). J. Geophysical Research
- [3] Liu (2000). Int. J. Heat Mass Transfer
- [4] Rivière & Soufiani (2012). Int. J. Heat Mass Transfer
- [5] Rivière (1992). J. Quant. Spectro. & Radiative Transfer

- ❖ YALES2 solves the RTE:
 - ❖ For a transparent media (surface to surface)
 - ❖ For a participating media in reordered k-space

- ❖ SNB-CK model based on EM2C latest database [1,2,3,4]

- ❖ Includes CO₂, H₂O, CO & CH₄

- ❖ No SGS Turbulent-Radiation Interaction

- ❖ Quadrature methods
 - ❖ Gauss-Lobato (7pts and 20pts)
 - ❖ Gauss-Legendre (2pts, 4pts and 7pts)
 - ❖ Gauss-Radau [5] (7pts)

- ❖ Optimized Brent Method to solve for k^* for each spectral quadrature point

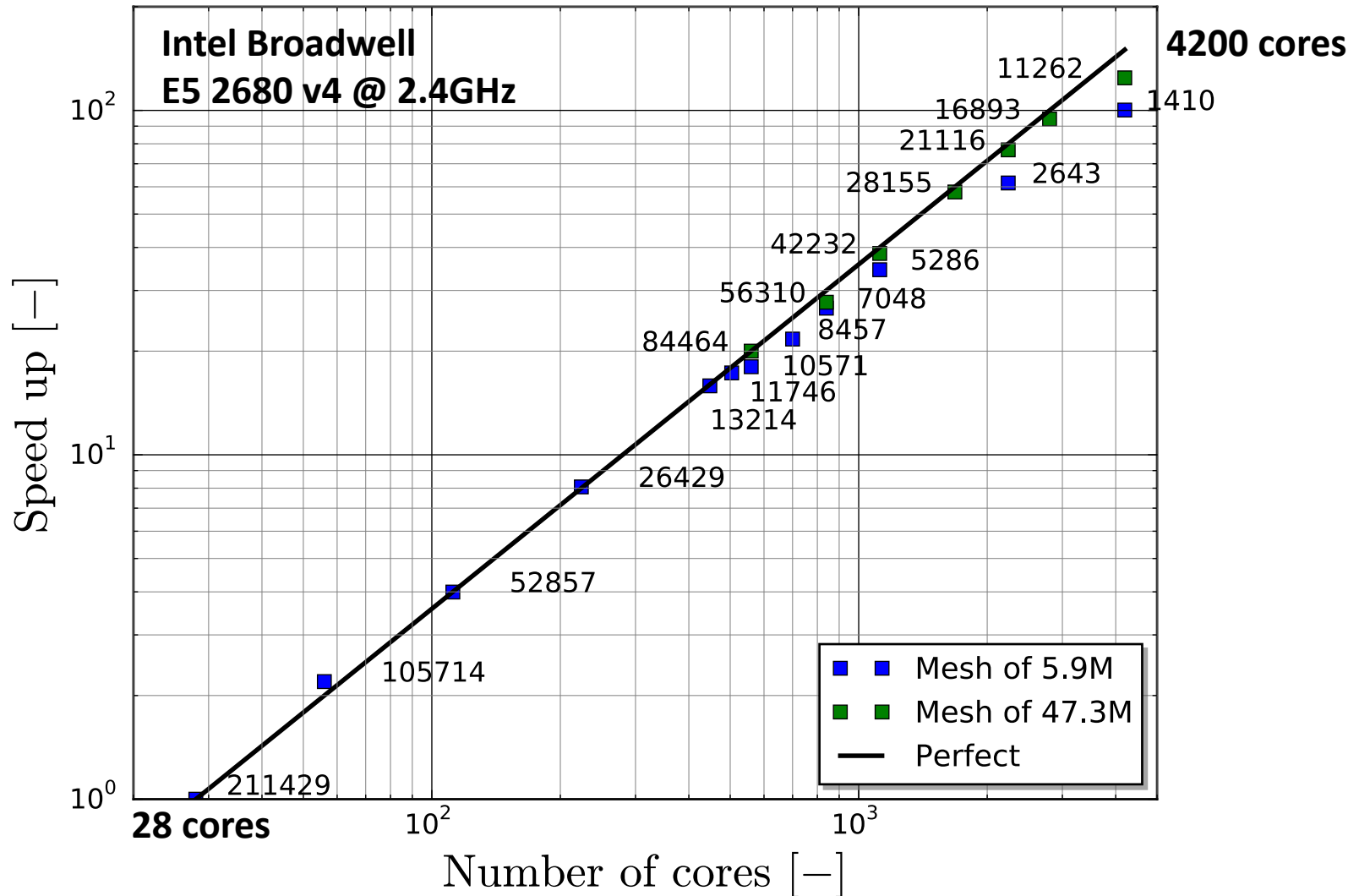
- ❖ Vectorized instructions to accelerate computations

- ❖ Low impact on CPU consumption

Radiative solver: DOM

- ❖ YALES2 solves the RTE with a DOM method
- ❖ In 2D: S4 (2 directions/quadrant) → S32 (16 directions/quadrant)
- ❖ In 3D: S4 (3 directions/octant)
- ❖ All directions are solved simultaneously:
 - ❖ without scattering: directions are decoupled (efficient)
 - ❖ with scattering: only minor modifications to the solver
- ❖ The RTE is discretised with a 4th order centred method with 10% upwinding
- ❖ Linear solver: optimized and fully vectorized parallel BiCG-Stab(2) [1]
- ❖ Very efficient: uses the SAME MESH as the fluid (tens of millions of cells)

HPC: performances of YALES2 radiative module



I. Model and coupling strategies

II. Academic validation



III. Torch flame topology

Academic validation test-case: INTRIG

[1] Miguel-Brebion (2016). Comb & Flame
[2] Xavier (2017). JFM
[3] Meija (2017). Proceedings Comb Inst
[4] Meija (2018). Comb & Flame

❖ INTRIG: experimental combustion chamber [1,2,3,4]

- Mixture: CH₄ and Air
- Laminarized flow
- **Combustion chamber:**
 - owns a cylindrical steel Bluff-body
 - stabilizes a V-flame

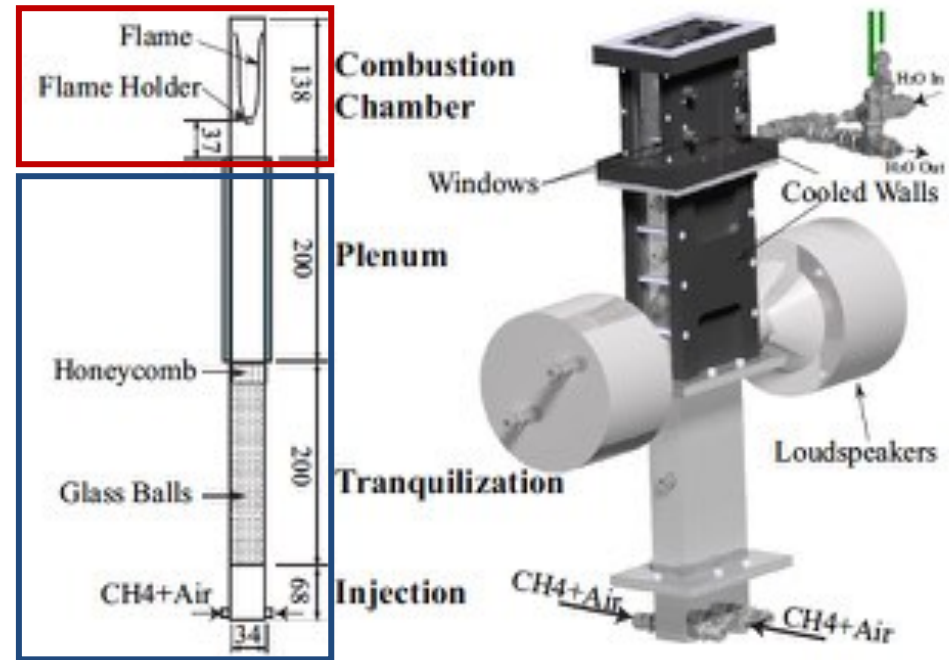
❖ Numerical parameters

- Fluid: air at $u \approx 1\text{m/s}$ ($Re = 584$)
- Flow with Von-Karman streets (40Hz)
- 2D Mesh: 630 000 tetrahedrons
 - $70\mu\text{m}$ in the flame and the solid
 - Prism layers of $20\mu\text{m}$ at interface

❖ Interest

- Validate CHT & radiation strategies
- Use radiation // present studies [1,2]

Part to simulate



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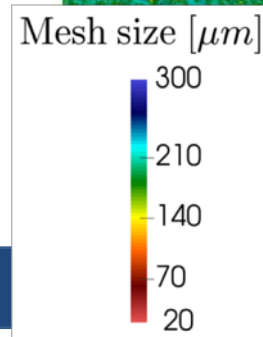
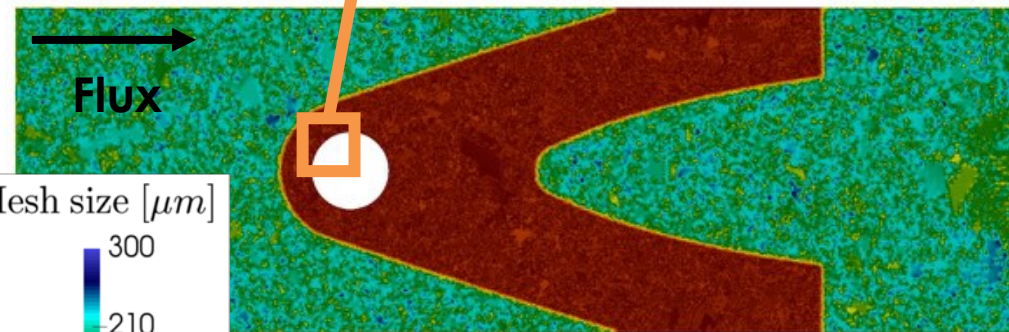
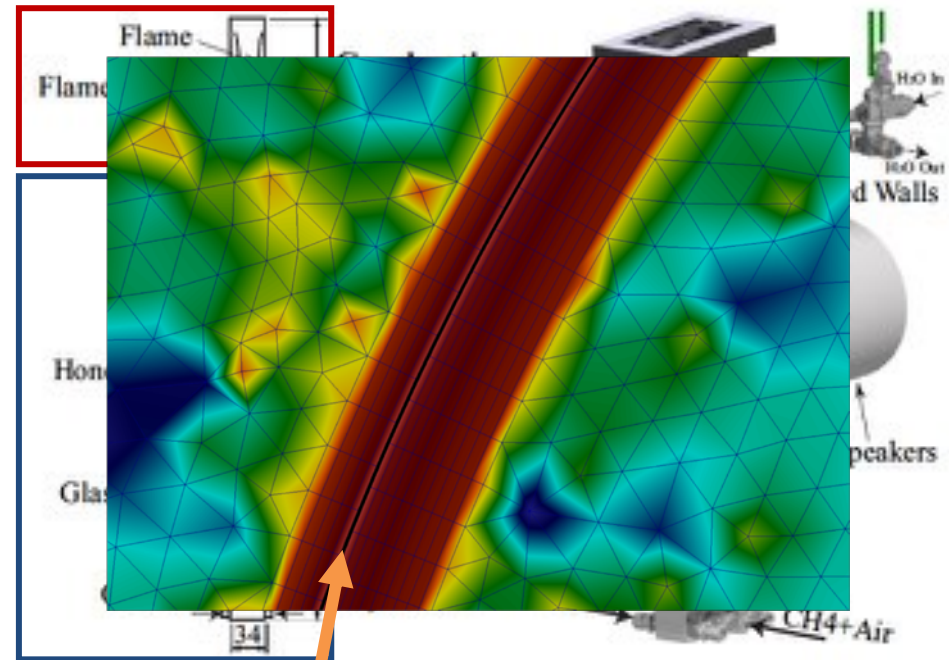
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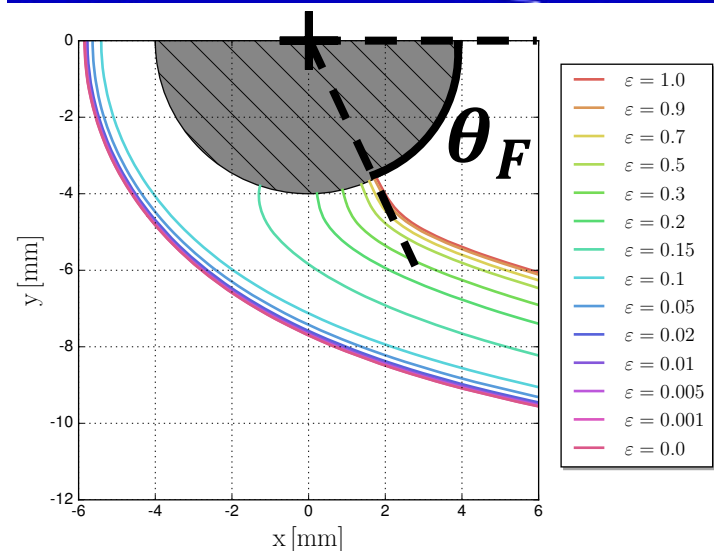
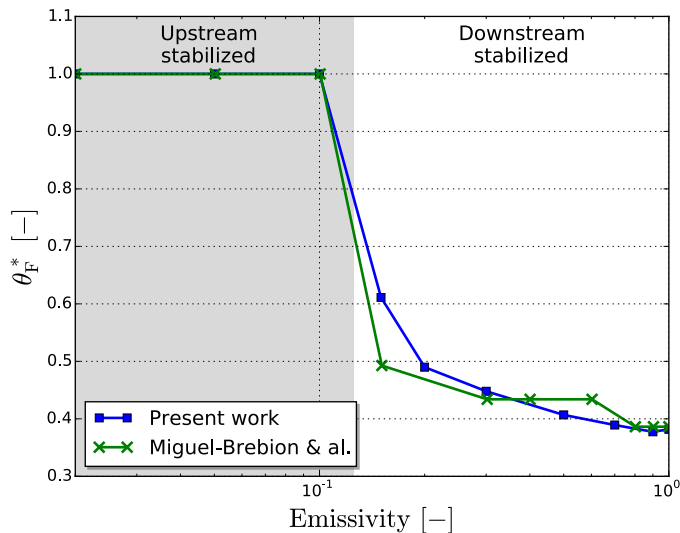
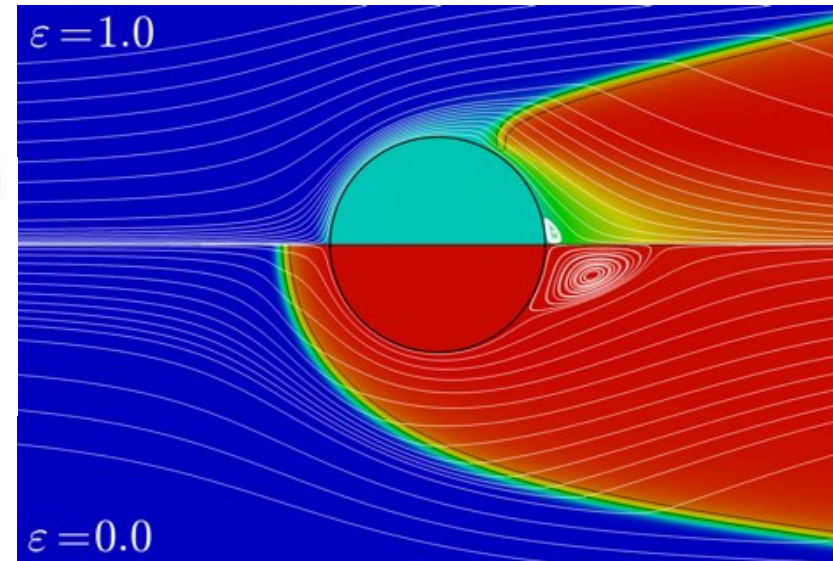
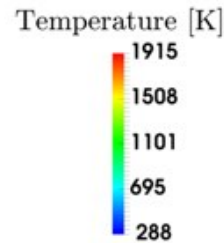
Academic validation test-case: Influence of cylinder emissivity

❖ 2 types of flame stabilisation

- $\varepsilon = 1$: downstream stabilized
 - Low T & little recirculation zone
- $\varepsilon = 0$: upstream stabilized
 - High T & large recirculation zone

❖ Angle profile

- Gap between $\varepsilon = 0.15$ and $\varepsilon = 0.1$
- Good comparison with [1]



Academic validation test-case: Influence of transparent & participative medium

❖ 2 possibilities of interactions for RHT

- Transparent medium: walls
 - Like in [1]
- Participative medium: walls + burnt gases
 - New approach

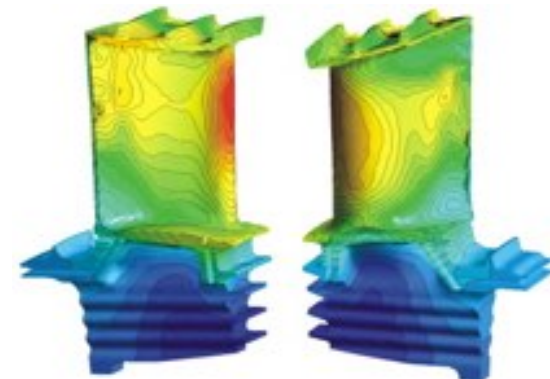
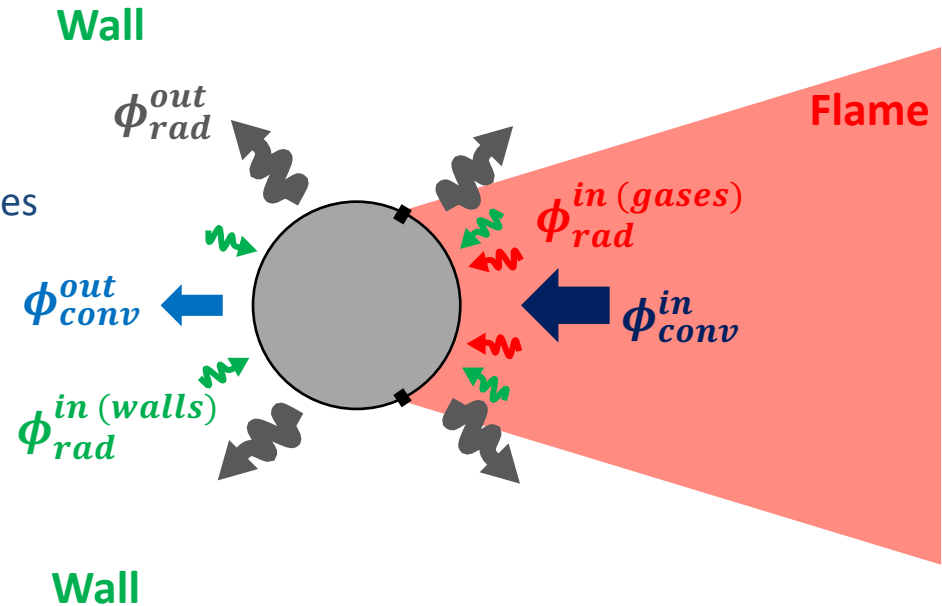
❖ Impact on the cylinder T

- Similar behaviour
- At $\varepsilon = 0$: $T = T_{adiab}$
- Difference up to 30K for high ε

❖ Is this T difference really important?

- In aeronautic field: **YES!**
- Prediction of T on turbine blade
 - Range of ε : between 0.6 and 0.9 [3]
- ↗ T of 30K ↘ Time Life by a factor of 9 [2]

High influence of Participative gases at high ε



Temperature profile [2],
from 700K (blue) to 1200K (red)

Academic validation test-case: Influence of transparent & participative medium

[1] Miguel-Brebion (2016). Comb & Flame
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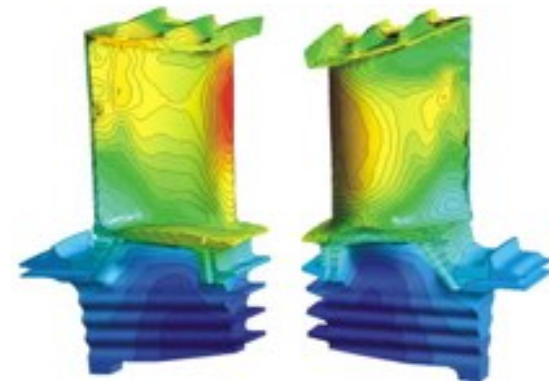
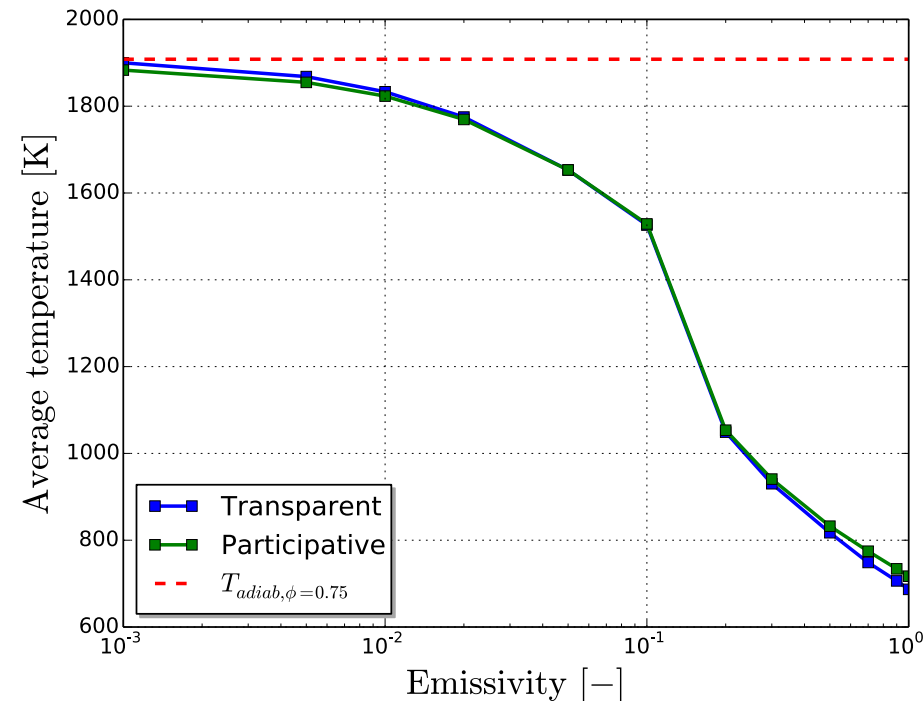
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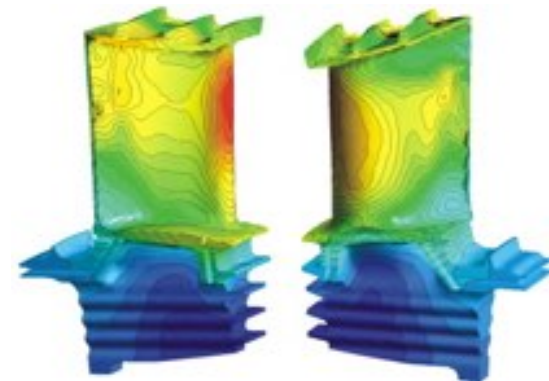
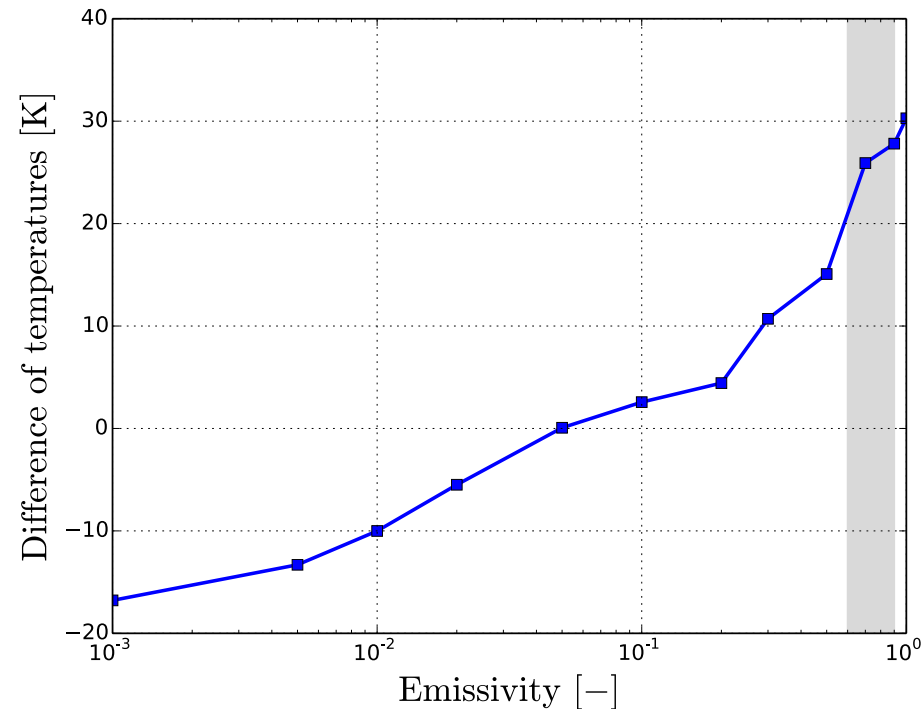
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Temperature profile [2],
from 700K (blue) to 1200K (red)

Academic validation test-case: Influence of angular discretisation

Radiative heat flux [W/m^2]

0 4075 8150 12225 16300



CHT and radiative strategy validated
➤ Application to torch modeling

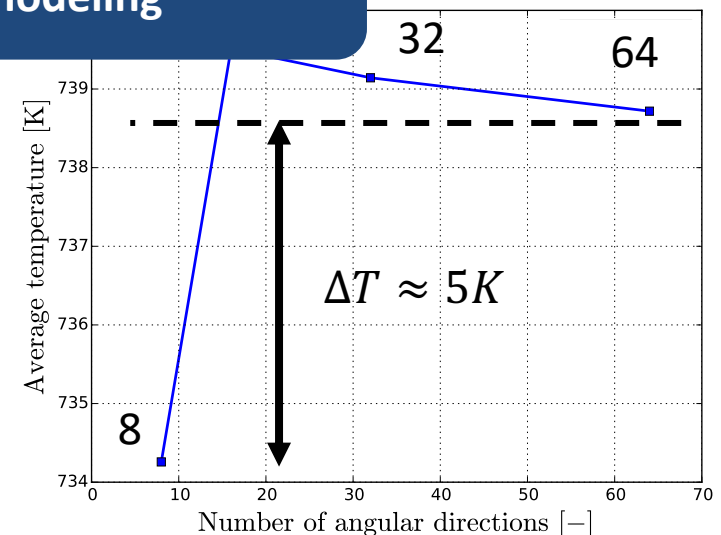
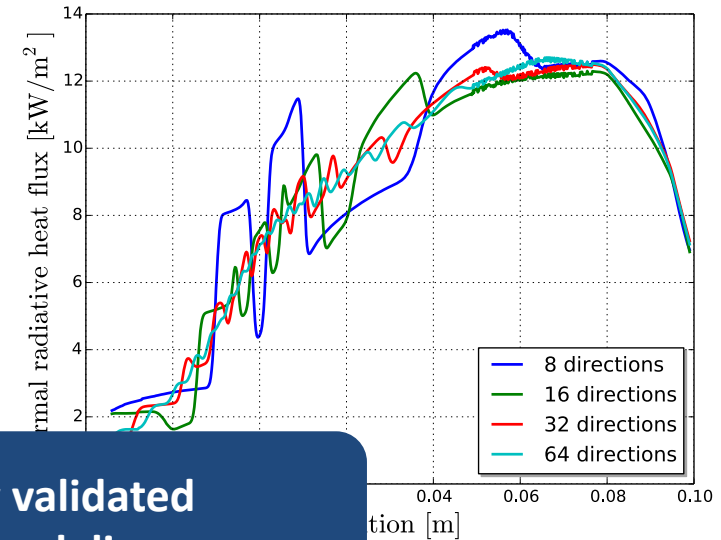
❖ Influence on wall

- $N_a = 8$ used until here
- + discretisation = - ray effects
- This can lead to major over/under-shoots on wall heat fluxes

❖ Influence on T_{cylinder} ($\epsilon = 0.9$)

- Convergence toward a stable T
- Difference of about 5K

Key role of Angular Discretisation for CHT



I. Model and coupling strategies

II. Academic validation

III. Torch flame analysis



Torch modeling strategy

❖ Multi-physic aspects



Spray



Evaporation



Flame

❖ Heat transfers



Convection



Conduction



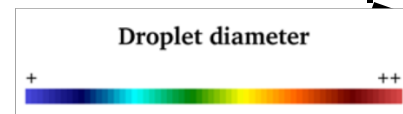
Radiation

1. Adiabatic

2. CHT +
Radiation

❖ Numerical parameters

- DOM: S4 → 24 directions
- Spectral quadrature: Gauss-Lobato with 7 pts
- $dt_{\text{fluid}} = 4.5\mu\text{s}$ $dt_{\text{solid}} = 29.2\mu\text{s}$



Turbulator

Cone



Torch modeling strategy

❖ Multi-physic aspects



Spray



Evaporation



Flame

❖ Heat transfers



Convection



Conduction



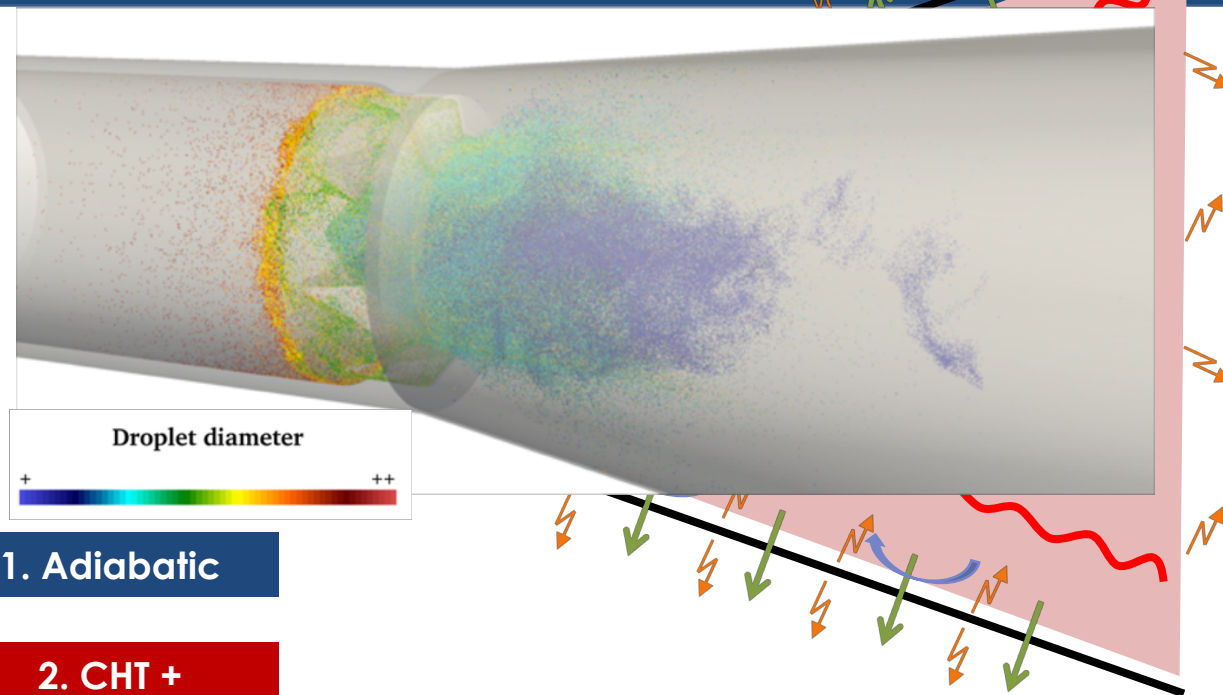
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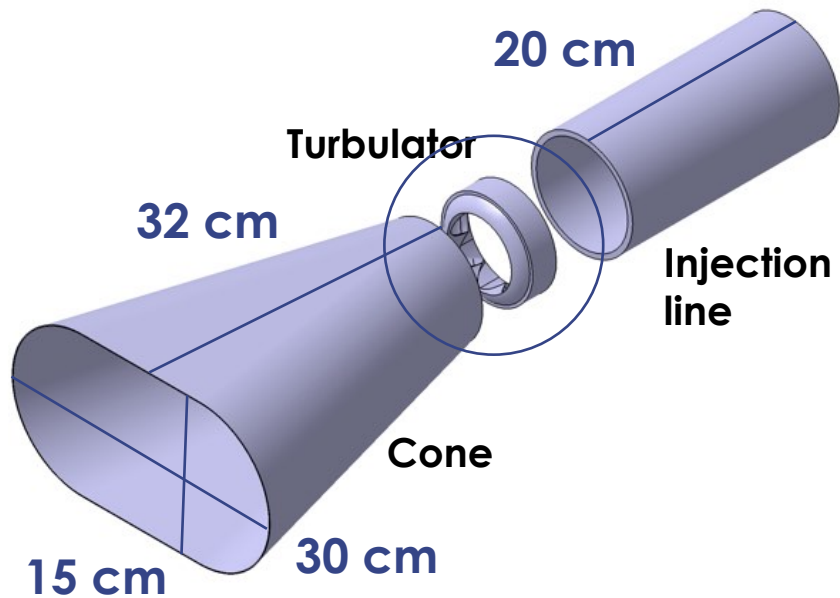
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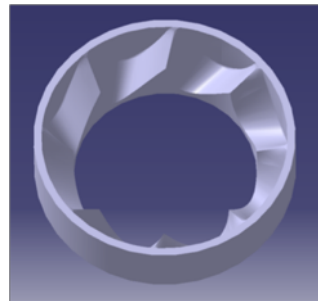
Geometry modeling



Turbulator:



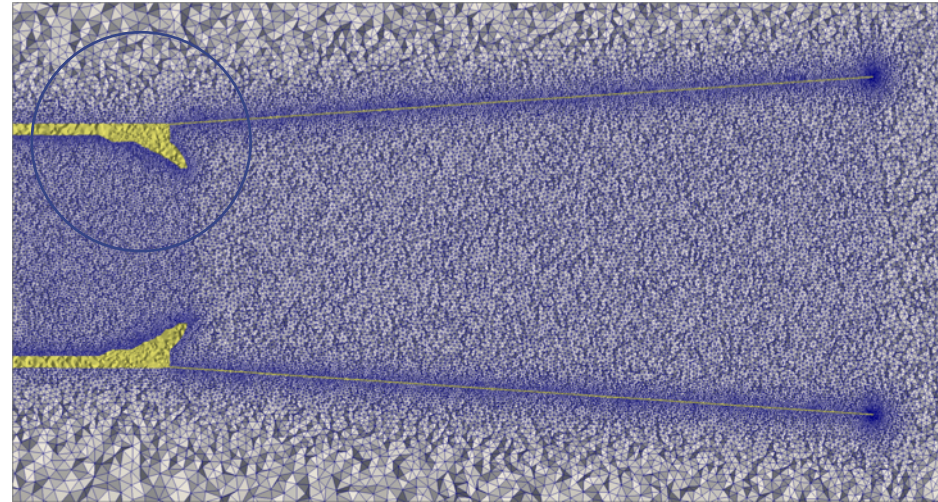
Front



Rear

Domain & mesh

Simulation domain $\approx 3m^3$

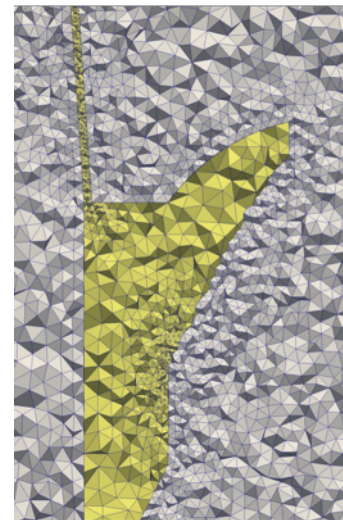


Fluid:

- From 0.4 to 2 mm
- Cell count: 40 M tets

Solid:

- From 0.2 to 1 mm
- Cell count: 140 M tets
thickness of the cone



CHT strategy: variables & solver interactions

[2] V. Moureau (2011). Combustion & Flame
 [3] http://www.cerfacs.fr/globc/PALM_WEB/
 [4] M.B. Giles (1997). Int. journal for num methods in fluids
 [5] F. Duchaine (2009). Int Journal of Heat & Fluid Flow
 [6] A. Felippa (2001). Comput. methods in appl. mech. & eng.

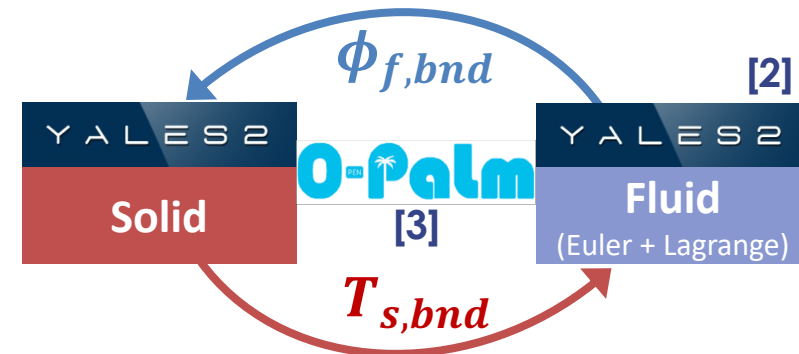
Fluid and **Solid** have to **communicate**

Solvers: YALES2

Coupling: **OpenPALM**

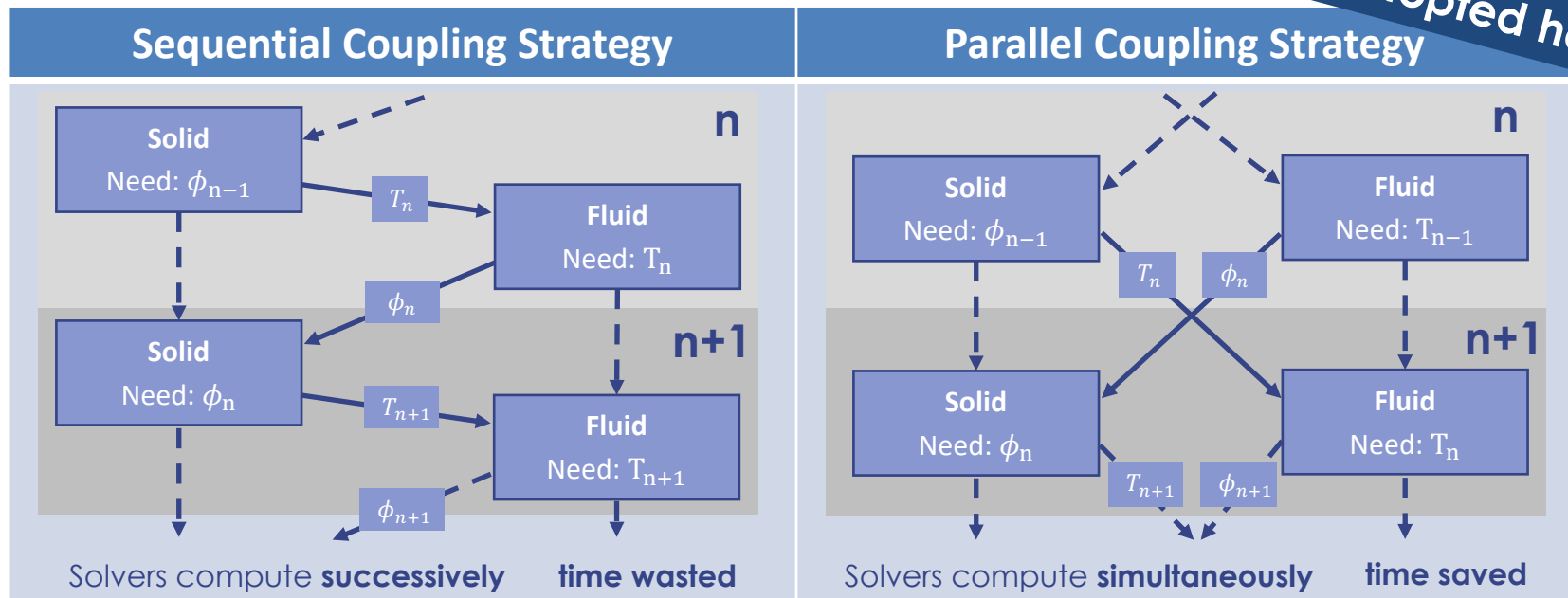
What is exchanged?

- Adopted here [4,5]
- **Fluid** side: **Flux** is sent
 - **Solid** side: **T** is sent



How is it exchanged ? [5,6]

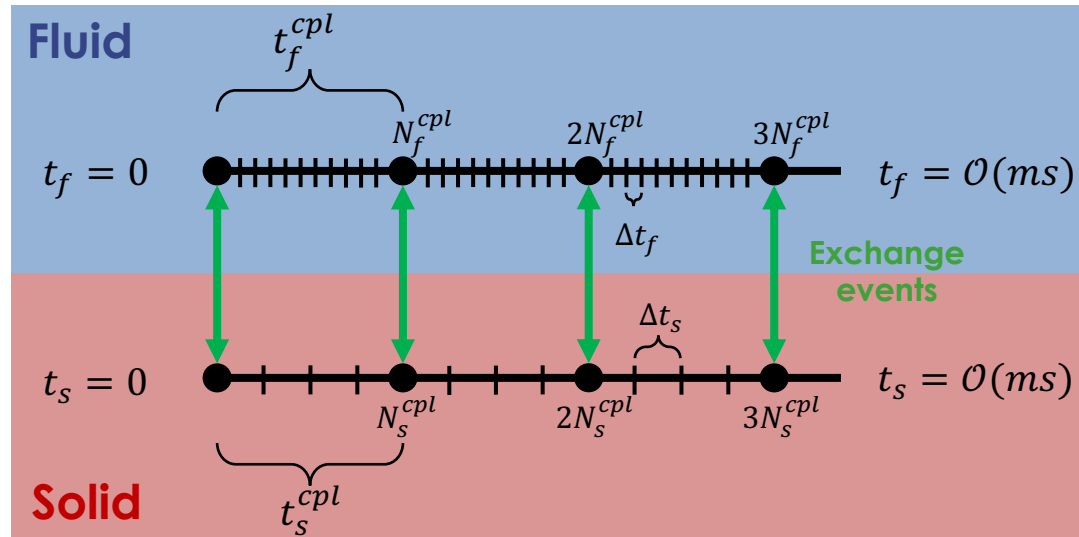
Adopted here



Coupling strategy: synchronisation time

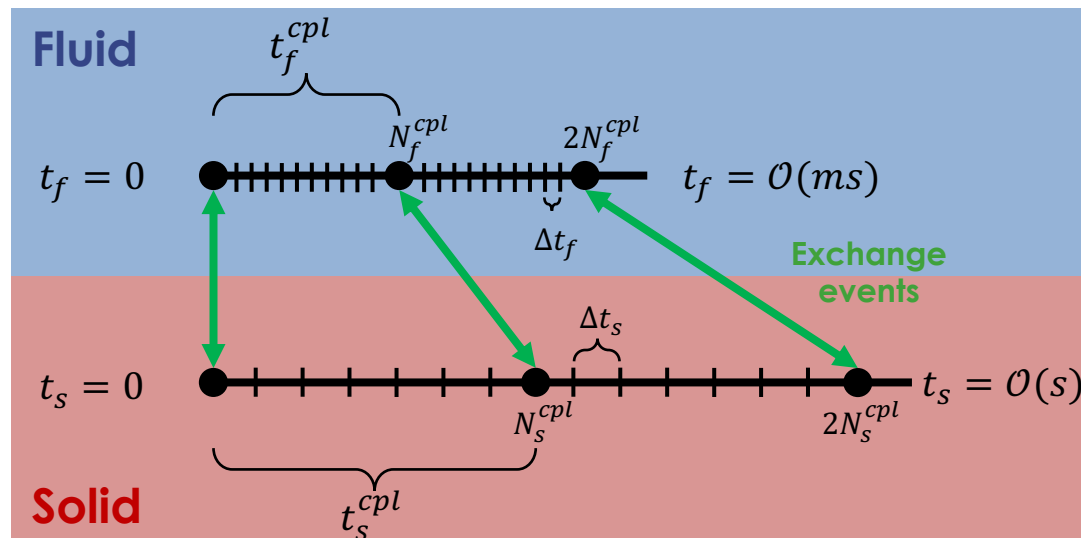
- **Synchronous coupled simulation:**

- Between exchange, the same physical time is computed by each solvers
- Time step of solid larger than time step of fluid
 - Waste of CPU time
 - Study transient state



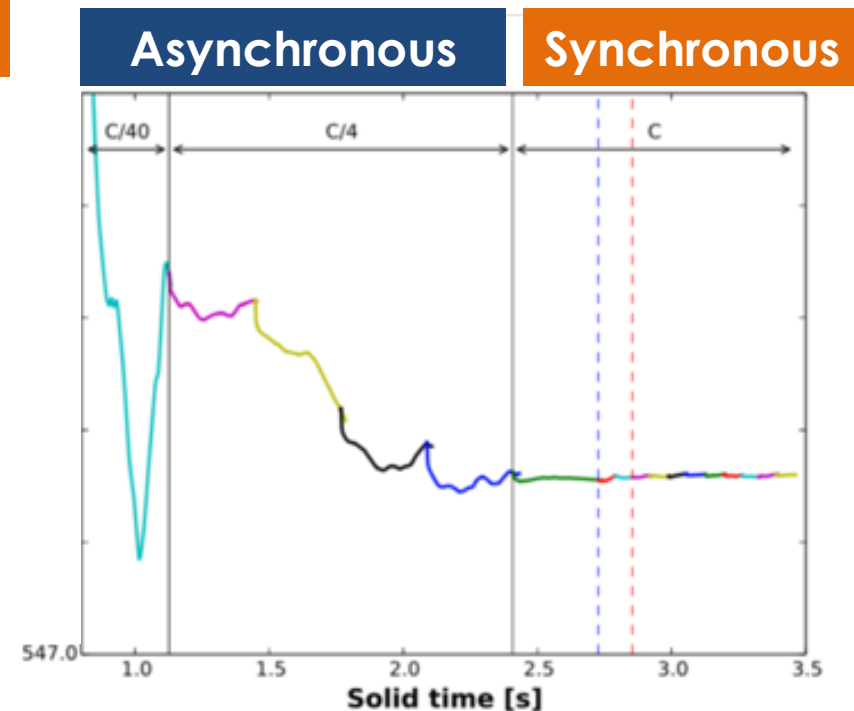
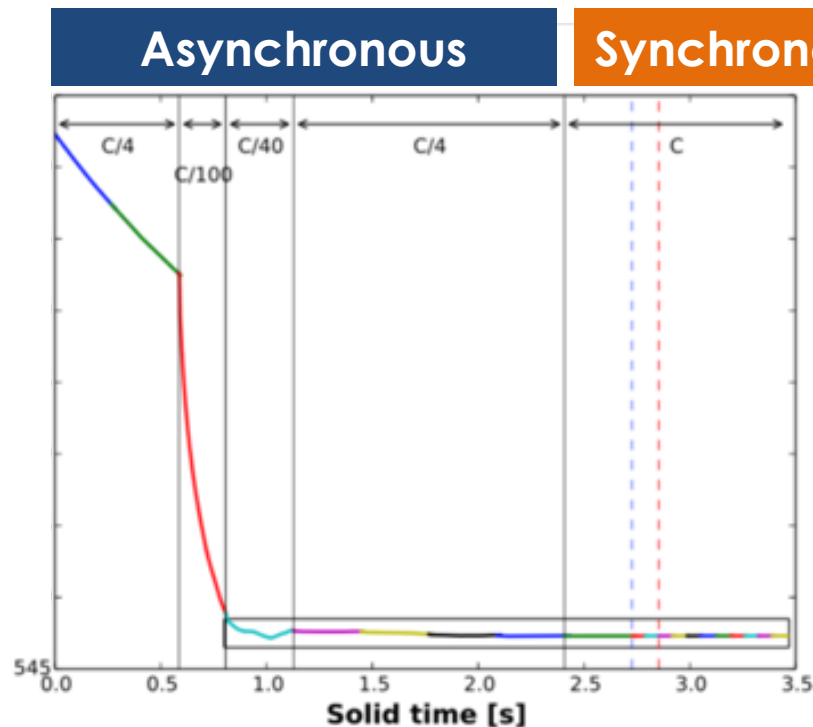
- **Asynchronous coupled simulation:**

- Between exchange, different physical times are computed by each solvers
- Bigger physical time can be computed in the solid
 - Waiting time reduced
 - Study converged state



Coupling strategy: improving convergence

- To reach steady-state
 - The heat capacity of the solid is artificially lowered
 - And then reset to its real value
same steady state
obtained much faster

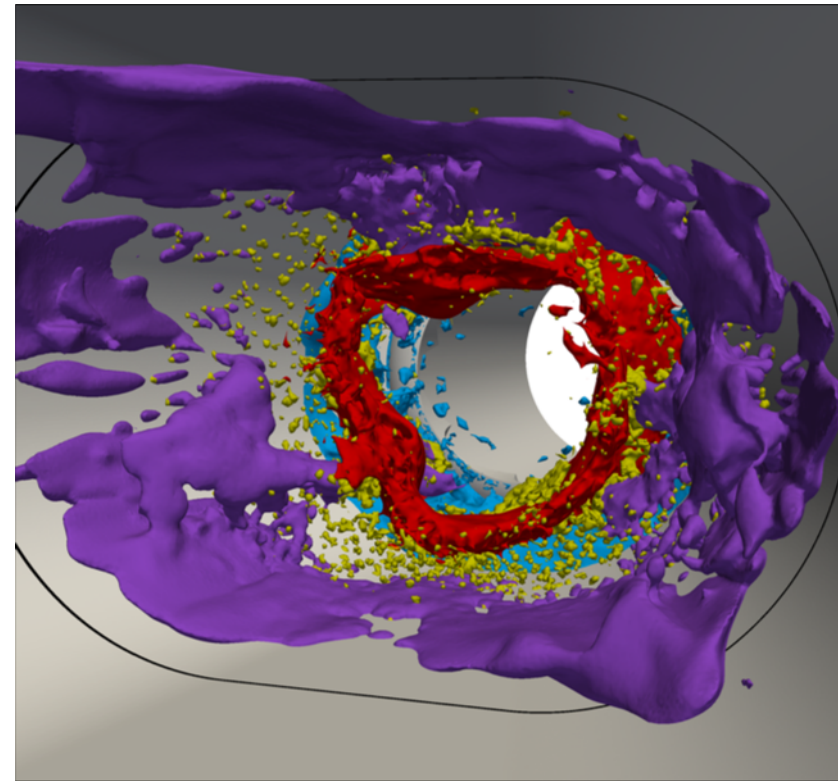
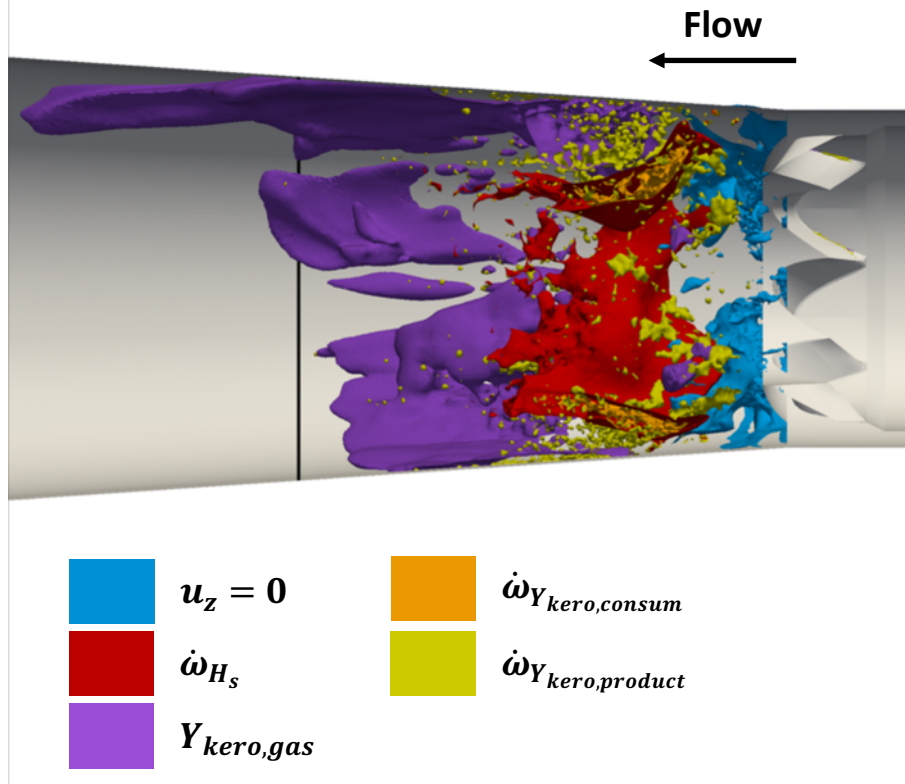
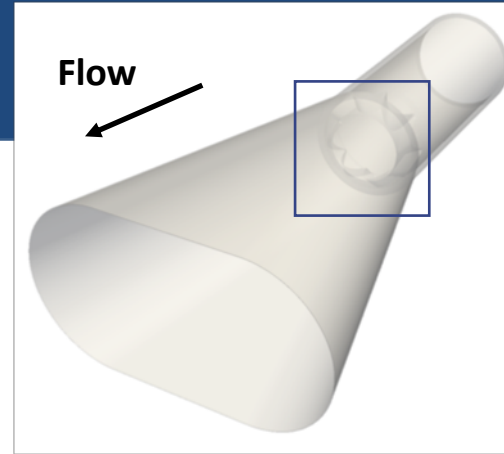


Coupling strategy: including Radiation

- Radiative solver invoked in the fluid phase before each coupling event
 - At each 32 iterations, i.e. each $144\mu\text{s}$.
 - On a 40M cells mesh, with S4 and 7pts quadrature
 - Non-symmetric and ill-conditioned linear system
 - BiCG-Stab(2) with $\sim 1'200\text{M}$ DoF
 - On 1024 processors...
 - This represents $\sim 40\%$ of total CPU time
-
- For simulations of transparent media, radiation = 2% of total CPU time

Topology of the flame: adiabatic case

- **Corner recirculation zone**
- **High values of fuel consumption where the flame is the strongest**
- **Large-scale flame wrinkling due to the turbulator**
- **Individual droplet evaporation at the wall and group droplet evaporation in the center**
- **Gaseous kerosene found at the wall due to large droplets crossing the flame**



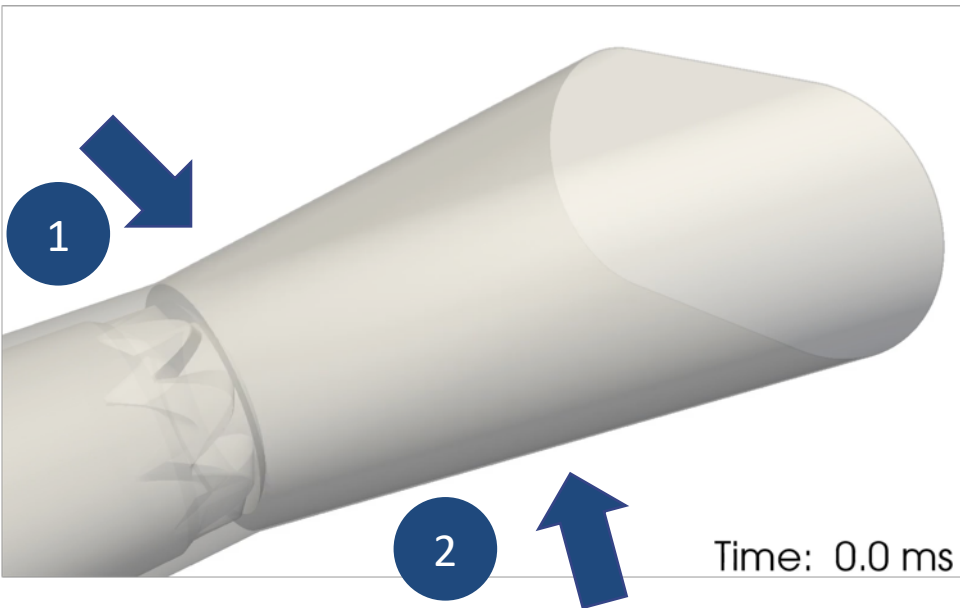
Topology of the flame inside the torch

Analysis of hot air plumes above the cone



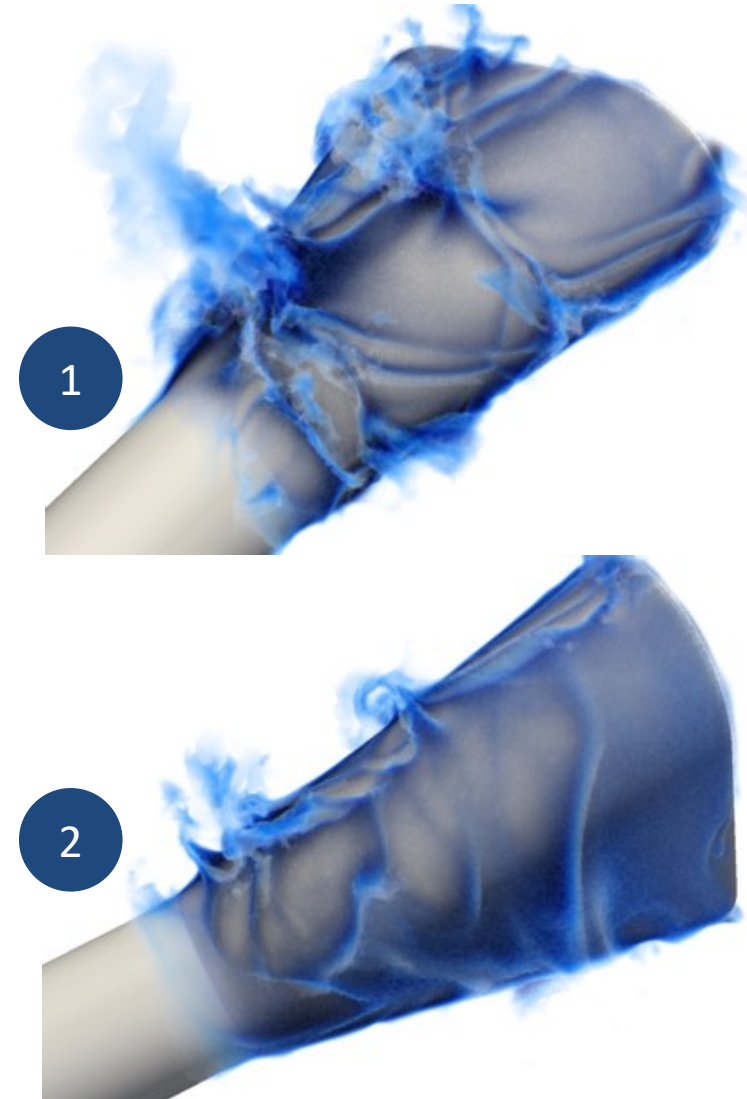
❖ Rendering of high values of $\dot{\omega}_T$ during 20ms

- Wrinkling due to the turbulator
- Isolated hot spots: combustion of droplets

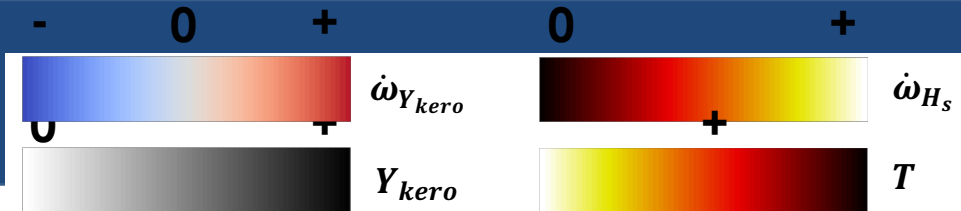


❖ Rendering of T in the air

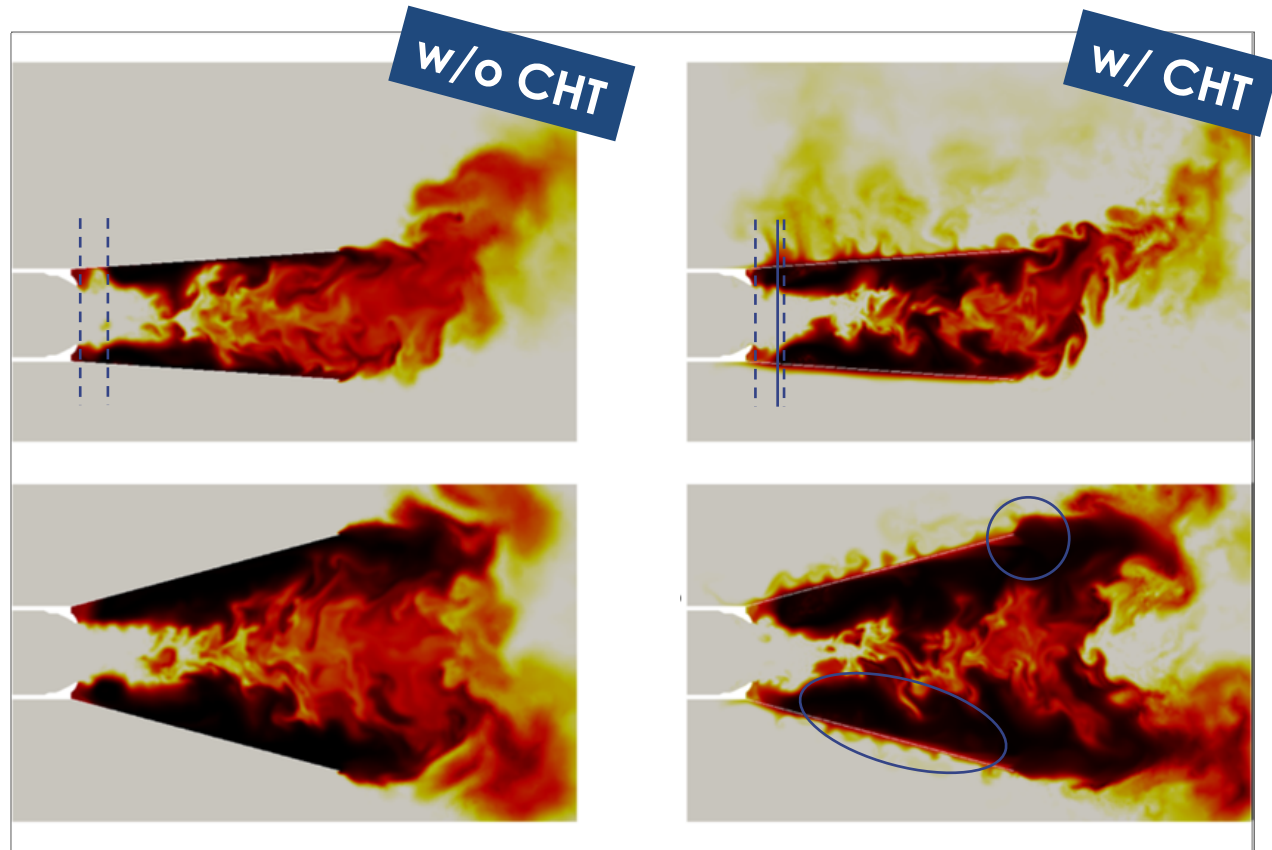
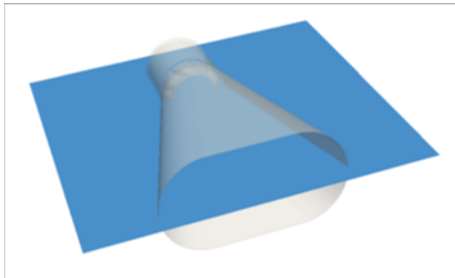
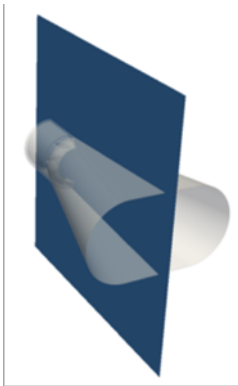
- CHT + Radiation in participative medium
- Upper side: natural convection driven by T gradient at the torch wall ($R_a = 6.10^6$)
- Lower side: quite stable stratification



Topology of the flame: adiabatic vs CHT



- Droplet evaporation starts upstream of the flame
- w/ CHT: consumption at the wall & the outlet
- w/ CHT: presence of gaseous kerosene on the walls
- Flame lift-off more important w/o CHT
- Hotter recirculation zones
- Large-scale flame wrinkling unaffected by CHT
- Hot air plume above the cone



Temperature profiles

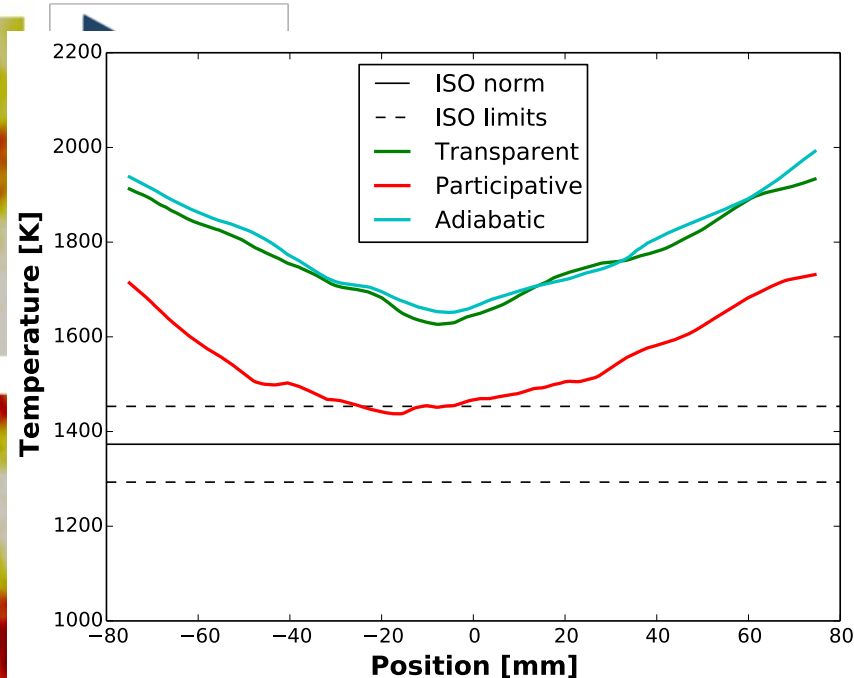
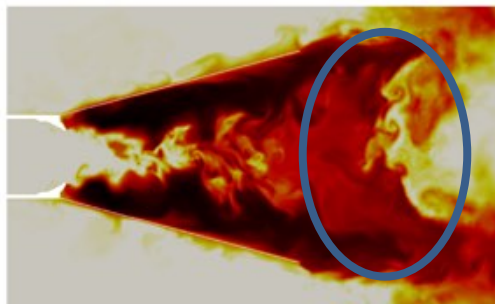
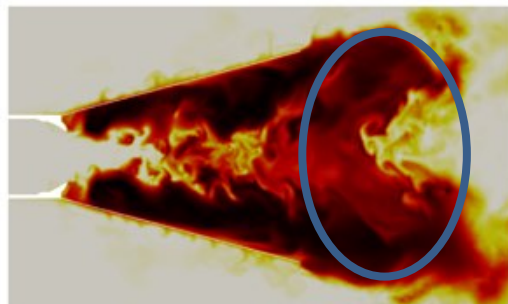


❖ Instantaneous temperature fields

- Seems to be lower with participative gases

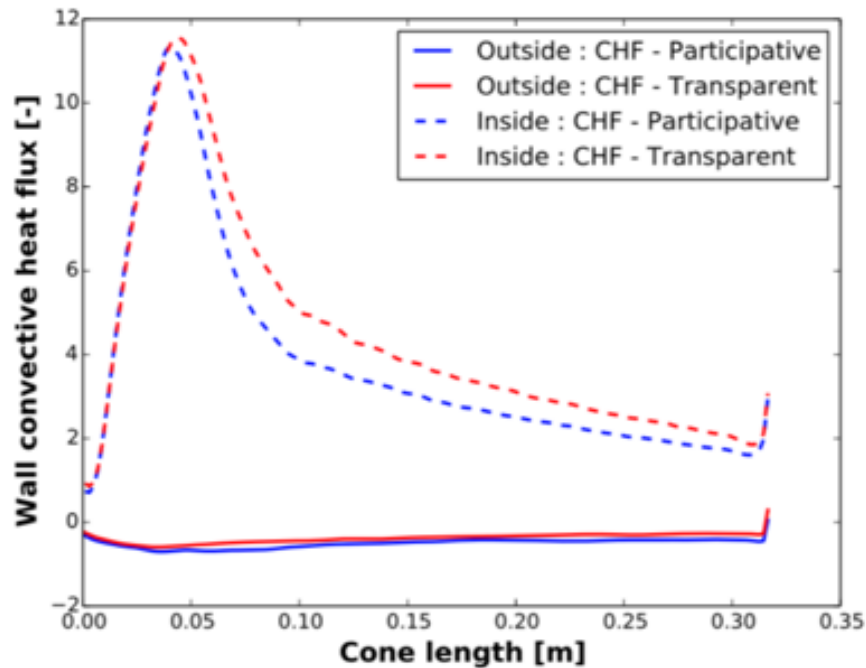
❖ Mean temperature at the outlet

- Adiabatic: too high values
- Transparent: same level as adiab. case
- Participative: $\approx 200\text{ K}$ lower \rightarrow almost at ISO values
 - Too simple chemistry (2 reactions)
 - Any models for soot formation

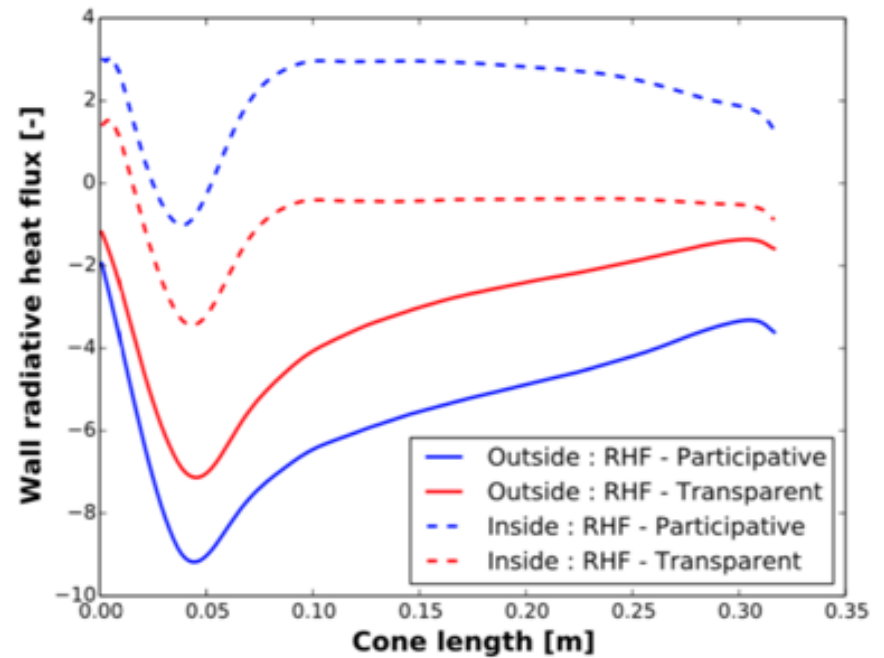


Fluxes at walls

Paroi	Interne		Externe	
Pertes thermiques	Convection	Rayonnement	Convection	Rayonnement
Transparent (%)	90.6	-9.4	15.1	84.9
Participative (%)	62.6	37.4	11.3	88.7

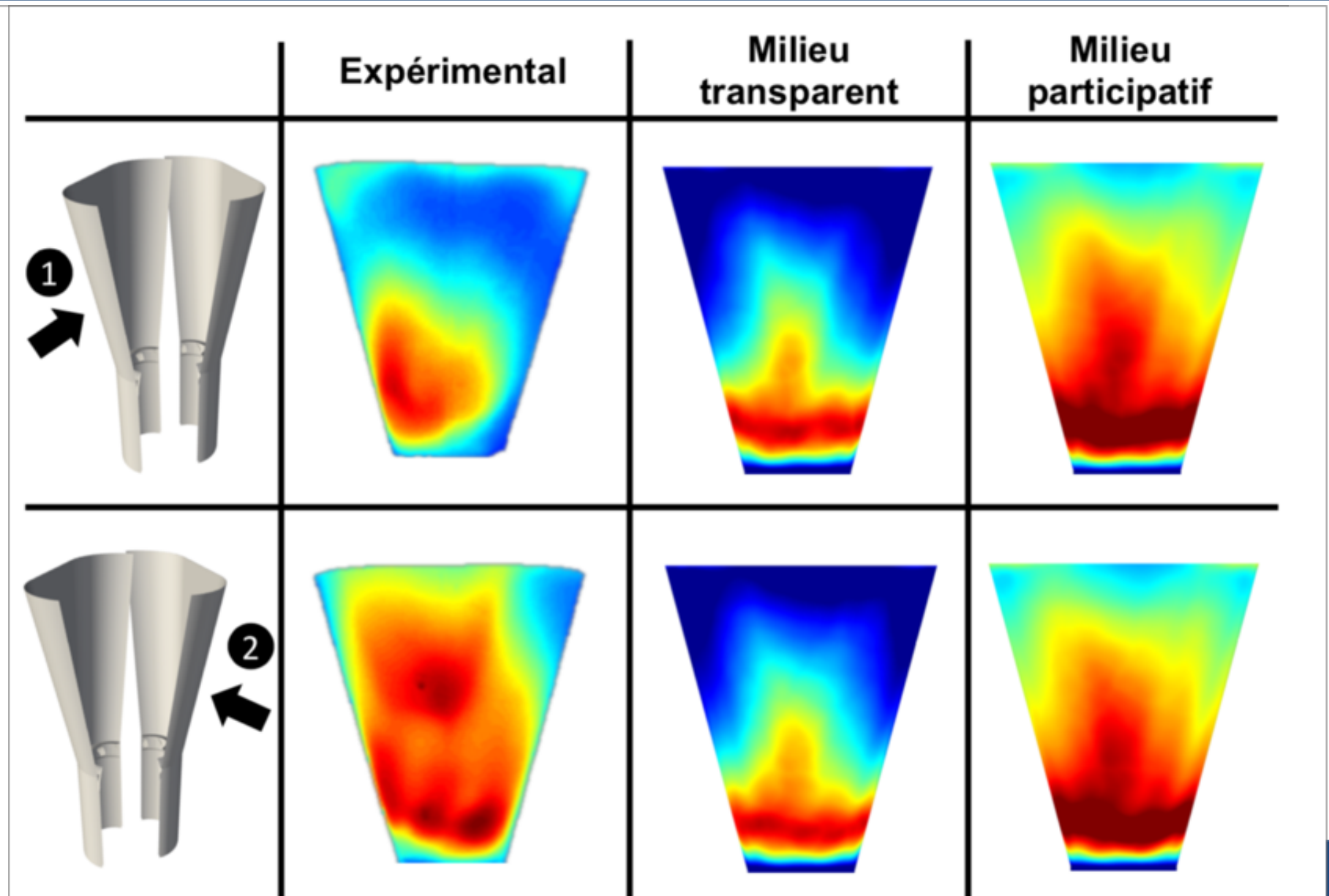


(a) Flux convectif



(b) Flux radiatif

External wall temperatures



Conclusion & perspectives

❖ INTRIG allowed to validate CHT & Radiation strategies

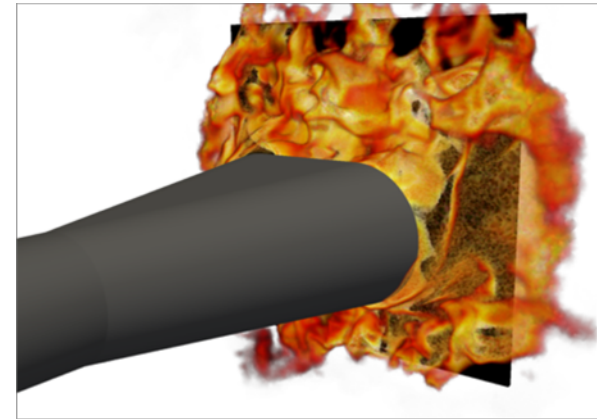
- Numerical results well reproduce with literature
- Number of ang. directions can have an impact when doing CHT

❖ In hot gases, influence of participative medium is vital

- To lower the gases temperature
- To predict good levels of temperature at the outlet of the torch

❖ What to do next?

- Comparison of T & ϕ on plane plate with exp. results
- Simulate a real certification test with engine envelope
- Include soot model and scattering



See you on December 20th at CORIA
for Lancelot Ph.D. defense!

